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## Economic Commission for Europe

### Inland Transport Committee

### World Forum for Harmonization of Vehicle Regulations

#### 191st session

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Item 4.8.6 of the provisional agenda

#### 1958 Agreement:

Consideration of draft amendments to existing

UN Regulations submitted by GRSP

## Proposal for 02 series of amendments to UN Regulation No. 134 (Hydrogen and Fuel Cells Vehicles)

### Submitted by the Working Party on Passive Safety \*

The text reproduced below was adopted by the Working Party on Passive Safety (GRSP) at its seventy-third session (ECE/TRANS/WP.29/GRSP/73 para. 37). It is based on ECE/TRANS/WP.29/GRSP/2023/8 as amended by GRSP-73-54. It is submitted to the World Forum for Harmonization of Vehicle Regulations (WP.29) and to the Administrative Committee (AC.1) for consideration at their November 2023 sessions

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\* In accordance with the programme of work of the Inland Transport Committee for 2023 as outlined in proposed programme budget for 2023 (A/77/6 (Sect. 20), table 20.6), the World Forum will develop, harmonize and update UN Regulations in order to enhance the performance of vehicles. The present document is submitted in conformity with that mandate.



*Reference to Consolidated Resolution on the Construction of Vehicles (R.E.3.), in all the text of the UN Regulation, amend to read:*

"As defined in the Consolidated Resolution on the Construction of Vehicles (R.E.3.), document ECE/TRANS/WP.29/78/Rev.7, ... - <https://unece.org/transport/standards/transport/vehicle-regulations-wp29/resolutions>"

*Paragraph 1, Footnote 1, amend to read:*

"<sup>1</sup> This Regulation does not cover the electrical safety of electric power train, the material compatibility and hydrogen embrittlement of the vehicle fuel system, and the post crash fuel system integrity in the event of rear impact."

*Paragraphs 1.2. to 1.3., amend to read:*

- "1.2. Part II - Specific components for compressed hydrogen storage systems for hydrogen-fuelled vehicles on their safety-related performance.
- 1.3. Part III Hydrogen-fuelled vehicles of category M and N<sup>2</sup> incorporating compressed hydrogen storage system on its safety-related performance."

*Paragraphs 2.2. to 2.4., amend to read:*

- "2.2. "Check valve" means a non-return valve that prevents reverse flow.
- 2.3. "Compressed hydrogen storage system (CHSS)" means a system designed to store compressed hydrogen fuel for a hydrogen-fuelled vehicle and composed of a container, container attachments (if any), and all primary closure devices required to isolate the stored hydrogen from the remainder of the fuel system and the environment.
- 2.4. "Container" (for hydrogen storage) means the pressure-bearing component on the vehicle that stores the primary volume of hydrogen fuel in a single chamber or in multiple permanently interconnected chambers."

*Insert new paragraphs 2.5., to read:*

- "2.5. "Container Attachments" mean non-pressure bearing parts attached to the container that provide additional support and/or protection to the container and that may be only temporarily removed for maintenance and/or inspection only with the use of tools."

*Paragraph 2.5. (former), renumber as paragraph 2.6.*

*Paragraphs 2.6.to 2.7. (former), renumber as paragraphs 2.7. to 2.8. and amend to read:*

- "2.7. "Date of manufacture" (of a compressed hydrogen container) means the date (month and year) of the proof pressure test or final inspection test carried out by the manufacturer.
- 2.8. "Enclosed or semi-enclosed spaces" means the special volumes within the vehicle (or the vehicle outline across openings) that are external to the hydrogen system (storage system, fuel cell system, internal combustion engine (ICE) and fuel flow management system)."

*Paragraph 2.8. (former), shall be deleted*

*Paragraph 2.12., amend to read:*

- "2.12. "Hydrogen-fuelled vehicle" means any motor vehicle that uses compressed gaseous hydrogen as a fuel to propel the vehicle, including fuel cell and internal combustion engine vehicles. Hydrogen fuel for the vehicles is specified in ISO 14687:2019 and SAE J2719\_202003."

*Paragraphs 2.15. to 2.17., amend to read:*

- "2.15. "Maximum allowable working pressure (MAWP)" means the highest gauge pressure to which a container or hydrogen storage system is permitted to operate under normal operating conditions.

- 2.16. "Maximum fuelling pressure (MFP)" means the maximum pressure applied to compressed hydrogen storage system during fuelling. The maximum fuelling pressure is 125 per cent of the Nominal Working Pressure.
- 2.17. "Nominal working pressure (NWP)" means the gauge pressure that characterizes typical operation of a system. For compressed hydrogen storage system, NWP is the settled pressure of compressed gas in fully fuelled container at a uniform temperature of 15 °C."

Insert new paragraphs 2.18., to read:

- "2.18. "Passenger compartment" means the space for occupant accommodation, bounded by the roof, floor, side walls, doors, outside glazing, front bulkhead and rear bulkhead or rear gate."

Paragraph 2.18. (former), renumber as paragraph 2.19.

Insert new paragraphs 2.20., to read:

- "2.20. "Rechargeable electrical energy storage system (REESS)" means the rechargeable energy storage system that provides electric energy for electrical propulsion."

Paragraph 2.19. (former), renumber as paragraph 2.21.

Paragraph 2.20.(former), shall be deleted.

Paragraph 2.21.(former), renumber as paragraph 2.22.

Paragraphs 2.22.to 2.23. (former), renumber as paragraphs 2.23. to 2.24. and amend to read:

- "2.23. "Shut-off valve" means a valve between the container and the vehicle fuel system that must default to the "closed" position when not connected to a power source.
- 2.24. "Single failure" means a failure caused by a single event, including any consequential failures resulting from this failure."

Insert new paragraphs 2.25. to 2.26., to read:

- "2.25. "Specific Heat Release Rate (HRR/A)" means the heat release from a fire per unit area of the burner where the heat release is based on the rate of fuel being combusted multiplied by the lower heating value (LHV) of the fuel. The LHV (sometimes called the Net Heating Value) is appropriate for the characterization of vehicle fires since the product water from combustion remains a vapour. The LHV is approximately 46 MJ/kg but needs to be determined at each site based on the actual LPG composition.
- 2.26. "State of charge (SOC)" means the density ratio of hydrogen in the CHSS between the actual CHSS condition and that at NWP with the CHSS equilibrated to 15 °C. SOC is expressed as a percentage using the formula:

$$SOC(\%) = \frac{\rho(P, T)}{\rho(NWP, 15^{\circ}C)} \times 100$$

The density of hydrogen at different pressure and temperature are listed in the Table 1 below.

Table 1  
Compressed Hydrogen Density (g/l)

Temperature (°C)	Pressure (MPa)												
	1	10	20	30	35	40	50	60	65	70	75	80	87.5
-40	1.0	9.7	18.1	25.4	28.6	31.7	37.2	42.1	44.3	46.1	48.4	50.3	53.0
-30	1.0	9.4	17.5	24.5	27.7	30.6	36.0	40.8	43.0	45.1	47.1	49.0	51.7
-20	1.0	9.0	16.8	23.7	26.8	29.7	35.0	39.7	41.9	43.9	45.9	47.8	50.4
-10	0.9	8.7	16.2	22.9	25.9	28.7	33.9	38.6	40.7	42.8	44.7	46.6	49.2
0	0.9	8.4	15.7	22.2	25.1	27.9	33.0	37.6	39.7	41.7	43.6	45.5	48.1
10	0.9	8.1	15.2	21.5	24.4	27.1	32.1	36.6	38.7	40.7	42.6	44.4	47.0
15	0.8	7.9	14.9	21.2	24.0	26.7	31.7	36.1	38.2	40.2	42.1	43.9	46.5

20	0.8	7.8	14.7	20.8	23.7	26.3	31.2	35.7	37.7	39.7	41.6	43.4	46.0
30	0.8	7.6	14.3	20.3	23.0	25.6	30.4	34.8	36.8	38.8	40.6	42.4	45.0
40	0.8	7.3	13.9	19.7	22.4	24.9	29.7	34.0	36.0	37.9	39.7	41.5	44.0
50	0.7	7.1	13.5	19.2	21.8	24.3	28.9	33.2	35.2	37.1	38.9	40.6	43.1
60	0.7	6.9	13.1	18.7	21.2	23.7	28.3	32.4	34.4	36.3	38.1	39.8	42.3
70	0.7	6.7	12.7	18.2	20.7	23.1	27.6	31.7	33.6	35.5	37.3	39.0	41.4
80	0.7	6.5	12.4	17.7	20.2	22.6	27.0	31.0	32.9	34.7	36.5	38.2	40.6
85	0.7	6.4	12.2	17.5	20.0	22.3	26.7	30.7	32.6	34.4	36.1	37.8	40.2

"

*Paragraphs 2.24.to 2.28. (former), renumber as paragraphs 2.27. to 2.31.*

*Paragraph 3.1.2., amend to read:*

"3.1.2. A model of information document is shown in Annex 1, Part 1, Model--I."

*Paragraph 3.2.2., amend to read:*

"3.2.2. A model of information document is shown in Annex 1, Part 1, Model -II."

*Paragraph 5., amend to read:*

## **"5. Part I – Specifications of the compressed hydrogen storage system**

This part specifies the requirements for the compressed hydrogen storage system.

- (a) The primary closure devices shall include the following functions, which may be combined:
  - (i) TPRD;
  - (ii) Check valve; and
  - (iii) Shut-off valve
- (b) The primary closure devices shall be mounted directly on or within each container.
- (c) The CHSS shall meet the performance test requirements summarized in Table 2. The corresponding test procedures are specified in Annex 3.
- (d) All new compressed hydrogen storage systems produced for on-road vehicle service shall have a NWP of 70 MPa or less.
- (e) The service life of the CHSS shall be determined by the manufacturer, who shall establish the date of removal from the service taking account of the performance requirements applied in the respective market.

Table 2

### **Overview of performance requirements**

<i>Requirement section</i>	<i>Test article</i>
5.1. Verification tests for baseline metrics	Container or container plus container attachments, as applicable
5.2. Verification test for performance durability	Container or container plus container attachments as applicable
5.3. Verification test for expected on-road performance	CHSS
5.4. Verification test for service terminating performance in fire	CHSS
5.5. Verification test for closure durability	Primary closure devices

"

*Paragraphs 5.1.1. to 5.4., amend to read:*

"5.1.1. Baseline initial burst pressure

Three (3) containers shall be hydraulically pressurized until burst in accordance with Annex 3, paragraph 2.1. The container attachments, if any, shall also be included in this test, unless the manufacturer can demonstrate that the container attachments do not affect the test results and are not affected by the test procedure. The manufacturer shall supply documentation (measurements and statistical analyses) that establish the midpoint burst pressure of new containers,  $BP_0$ .

All containers tested shall have a burst pressure within  $\pm 10$  per cent of  $BP_0$  and greater than or equal to a minimum  $BP_{min}$  of 200 per cent NWP.

Containers having glass-fibre composite as a primary constituent shall have a minimum burst pressure greater than 350 per cent NWP.

5.1.2. Baseline initial pressure cycle life

Three (3) containers shall be hydraulically pressure cycled without rupture for 22,000 cycles or until a leak occurs in accordance with Annex 3, paragraph 2.2. The container attachments, if any, shall also be included in this test, unless the manufacturer can demonstrate that the container attachments do not affect the test results and are not affected by the test procedure. Leakage shall not occur within 11,000 cycles.

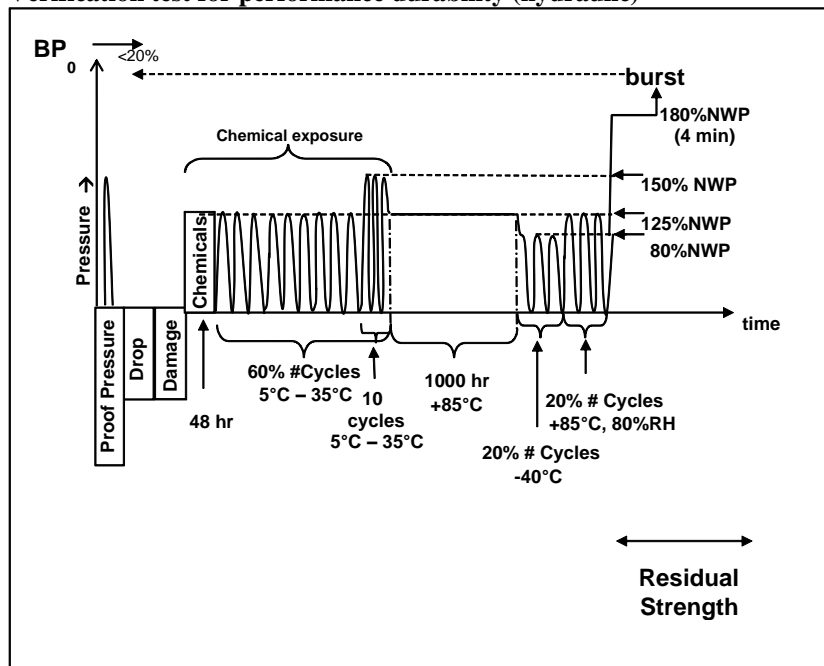
5.2. Verification tests for performance durability (Hydraulic sequential tests)

If all three pressure cycle life measurements made in paragraph 5.1.2. are greater than 11,000 cycles, or if they are all within  $\pm 25$  per cent of each other, then only one (1) container is tested in paragraph 5.2. Otherwise, three (3) containers are tested in paragraph 5.2.

Unless otherwise specified, the tests in paragraph 5.2 shall be conducted on the container equipped with its container attachments (if any) that represents the CHSS without the primary closures.

The container shall not leak during the following sequence of tests, which are applied in series to a single system and which are illustrated in Figure 1. Specifics of applicable test procedures are provided in Annex 3, paragraph 3.

Figure 1  
**Verification test for performance durability (hydraulic)**



5.2.1. Proof pressure test

The container is pressurized in accordance with the procedure specified in Annex 3, paragraph 3.1. The container attachments, if any, shall also be included in this test, unless the manufacturer can demonstrate that the container attachments do not affect the test results, and are not affected by the test procedure. The container that has undergone a proof pressure test in manufacture is exempt from this test.

5.2.2. Drop (impact) test

The container with its container attachments (if any) is dropped once in one of the impact orientations specified in Annex 3, paragraph 3.2.

5.2.3. Surface damage test

The container with its container attachments (if applicable) is subjected to surface damage specified in Annex 3, paragraph 3.3.

All-metal containers are exempt from the surface flaw generation portion of testing.

5.2.4. Chemical exposure and ambient-temperature pressure cycling test

The container with its container attachments (if applicable) is exposed to chemicals found in the on-road environment and pressure cycled in accordance with Annex 3, paragraph 3.4.

5.2.5. High temperature static pressure test.

The container with its container attachments (if applicable) is pressurized in accordance with Annex 3, paragraph 3.5. test procedure.

5.2.6. Extreme temperature pressure cycling test.

The container with its container attachments (if applicable) is pressure cycled in accordance with Annex 3, paragraph 3.6.

5.2.7. Residual proof pressure test.

The container with its container attachments (if applicable) is pressurized-in accordance with the procedure specified in Annex 3, paragraph 3.1.

## 5.2.8. Residual strength burst test

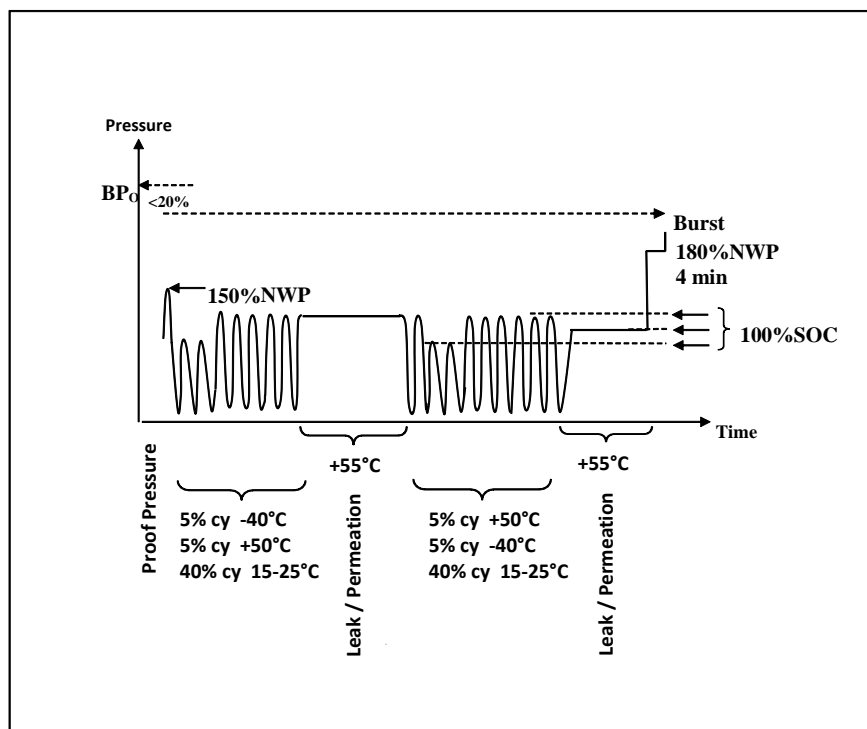
The container with its container attachments (if applicable) undergoes a hydraulic burst test. The burst pressure measured in accordance with the procedure specified in Annex 3, paragraph 2.1. shall be at least 80 per cent of the  $BP_0$  provided by the manufacturer in paragraph 5.1.1.

## 5.3. Verification test for expected on-road performance (Pneumatic sequential tests)

CHSS shall undergo the following sequence of tests, which are illustrated in Figure 2. Specifics of applicable test procedures for the CHSS are provided in Annex 3.

The CHSS shall not leak and the primary closure devices shall maintain functionality during the test.

Figure 2

**Verification test for expected on-road performance (pneumatic)**

## 5.3.1. Proof pressure test

The container of a CHSS is pressurized in accordance with the procedure specified in Annex 3, paragraph 3.1. The container attachments, if any, shall also be included in this test, unless the manufacturer can demonstrate that the container attachments do not affect the test results and are not affected by the test procedure. The container that has undergone a proof pressure test in manufacture may be exempted from this test.

## 5.3.2. Ambient and extreme temperature gas pressure cycling test (pneumatic)

CHSS is pressure cycled in accordance with Annex 3, paragraph 4.1.

## 5.3.3. Extreme temperature static gas pressure leak/permeation test (pneumatic).

The test shall be conducted in accordance with Annex 3, paragraphs 4.2. and 4.3.

The maximum allowable hydrogen discharge from the CHSS is 46 ml/hr/l water capacity of the CHSS. Any single point of localized external leakage

measured in accordance with Annex 3, paragraph 4.3. shall not exceed 0.005 mg/sec (3.6 Nml/min).

5.3.4. Residual proof pressure test (hydraulic)

The container with its container attachments (if any), as specified, is pressurized in accordance with the procedure specified in Annex 3, paragraph 3.1.

5.3.5. Residual strength burst test (hydraulic)

The container with its container attachments (if any), as specified, undergoes a hydraulic burst. The burst pressure measured in accordance with the procedure specified in Annex 3, paragraph 2.1. shall be at least 80 per cent of the BP<sub>O</sub> provided by the manufacturer in paragraph 5.1.1.

5.4. Verification test for service terminating performance in fire

The CHSS shall undergo the two-stage localized/engulfing fire test specified in Annex 3, paragraph 5.

The CHSS is filled to 100 per cent state-of-charge (SOC) with compressed hydrogen as the test gas.

The CHSS shall vent to less than 1 MPa within 1 hour for vehicles of categories M<sub>1</sub> and N<sub>1</sub> or within 2 hours for vehicles of categories M<sub>2</sub>, M<sub>3</sub>, N<sub>2</sub> and N<sub>3</sub>. If venting occurs from TPRD(s), the venting shall be continuous. The container shall not rupture during the CHSS fire test. Except for discharges from the exhausts of TPRD vents, any leakage, permeation, or venting from the CHSS, including through the container walls or joints, other components, and fittings, shall not result in jet flames greater than 0.5 m.

If the container pressure has not fallen below 1 MPa when the time limit defined above is reached, then fire testing is terminated and the CHSS fails the fire test (even if rupture did not occur)."

*Paragraphs 5.5. to 5.6., amend to read:*

"5.5. Requirements for primary closure devices

The primary closure devices that isolate the high pressure hydrogen storage system, namely TPRD, check valve and shut-off valve, shall be tested and type-approved in accordance with Part II of this Regulation and produced in conformity with the approved type.

Retesting of the CHSS is not required if alternative closure devices are provided having comparable function, fittings, materials, strength and dimensions, and satisfy the condition above. However, a change in TPRD hardware, its position of installation or venting lines shall require a new fire test in accordance with paragraph 5.4.

5.6. Labelling

A label shall be permanently affixed on each container or container attachments with at least the following information: name of the manufacturer, serial number, date of manufacture, MFP, NWP, type of fuel (e.g. "CHG" for gaseous hydrogen), and date of removal from service as well as the number of cycles used in the testing programme as per paragraph 5.1.2. Any label in compliance with this paragraph shall remain in place and be legible for the duration of the manufacturer's recommended service life for the container.

Date of removal from service shall not be more than 25 years after the date of manufacture."



*Paragraphs 6.1. to 6.2., amend to read:*

"6.1. TPRD requirements

TPRDs shall meet the following performance requirements:

- (a) Pressure cycling test (Annex 4, paragraph 1.1.);
- (b) Accelerated life test (Annex 4, paragraph 1.2.);
- (c) Temperature cycling test (Annex 4, paragraph 1.3.);
- (d) Salt corrosion resistance test (Annex 4, paragraph 1.4.);
- (e) Vehicle environment test (Annex 4, paragraph 1.5.);
- (f) Stress corrosion cracking test (Annex 4, paragraph 1.6.);
- (g) Drop and vibration test (Annex 4, paragraph 1.7.);
- (h) Leak test (Annex 4, paragraph 1.8.);
- (i) Bench top activation test (Annex 4, paragraph 1.9.);
- (j) Flow rate test (Annex 4, paragraph 1.10.);
- (k) Atmospheric exposure test (Annex 4, paragraph 1.11.).

6.2. Check valve and shut-off valve requirements

Check valves and shut-off valves shall meet the following performance requirements:

- (a) Hydrostatic strength test (Annex 4, paragraph 2.1.);
- (b) Leak test (Annex 4, paragraph 2.2.);
- (c) Extreme temperature pressure cycling test (Annex 4, paragraph 2.3.);
- (d) Salt corrosion resistance test (Annex 4, paragraph 2.4.);
- (e) Vehicle environment test (Annex 4, paragraph 2.5.);
- (f) Atmospheric exposure test (Annex 4, paragraph 2.6.);
- (g) Electrical tests (Annex 4, paragraph 2.7.);
- (h) Vibration test (Annex 4, paragraph 2.8.);
- (i) Stress corrosion cracking test (Annex 4, paragraph 2.9.);"

*Paragraph 7., amend to read:*

**"7. Part III – Specifications of a vehicle fuel system incorporating the compressed hydrogen storage system**

This part specifies requirements for the vehicle fuel system, which includes the CHSS, piping, joints, and components in which hydrogen is present. The CHSS included in the vehicle fuel system shall be tested and type-approved in accordance with Part I of this Regulation and produced in conformity with the approved type."

*Paragraphs 7.1.1.1. to 7.1.1.2., amend to read:*

"7.1.1.1. A compressed hydrogen fuelling receptacle shall prevent reverse flow to the atmosphere. Test procedure is in accordance with the leak test specified in Annex 4, paragraph 2.2.

7.1.1.2. A label shall be affixed close to the fuelling receptacle; for instance, inside a refilling hatch, showing the following information: fuel type (e.g. "CHG" for gaseous hydrogen), MFP, NWP, date of removal from service of containers. "

*Insert new paragraph 7.1.1.5., to read:*

"7.1.1.5. The geometry of the fuelling receptacle of compressed hydrogen gas vehicles shall conform to international standard ISO 17268:2020 and be compatible with specification H35, H35HF or H70 depending on its nominal working pressure and specific application."

*Paragraph 7.1.2., amend to read:*

"7.1.2. Over-pressure protection for the low-pressure system (Annex 5, paragraph 6. test procedure)

The hydrogen system downstream of a pressure regulator shall be protected against overpressure due to the possible failure of the pressure regulator. The set pressure of the overpressure protection device shall be lower than or equal to the maximum allowable working pressure for the appropriate section of the hydrogen system."

*Paragraphs 7.1.3.1. to 7.1.3.2., amend to read:*

"7.1.3.1. Pressure relief systems (Annex 5, paragraph 6. test procedure)

- (a) The outlet of the vent line, if present, for hydrogen gas discharge from TPRD(s) of the CHSS shall be protected from ingress of dirt and water (e.g. by a cap);
- (b) The hydrogen gas discharge from TPRD(s) of the CHSS shall be directed such that the hydrogen exhaust does not impinge upon:
  - (i) enclosed or semi-enclosed spaces;
  - (ii) any vehicle wheel housing;
  - (iii) hydrogen gas containers;
  - (iv) the vehicle's REESS.

7.1.3.2. Vehicle exhaust system (Annex 5, paragraph 4. test procedure)

At the vehicle exhaust system's point of discharge, the hydrogen concentration level shall:

- (a) Not exceed 4.0 per cent average by volume during any moving three-second time interval during normal operation including start-up and shut-down;
- (b) And not exceed 8.0 per cent at any time (Annex 5, paragraph 4. test procedure)."

*Paragraph 7.1.4.1., amend to read:*

"7.1.4.1. Hydrogen gas discharge, leakage and/or permeation from the vehicle fuel system shall not directly vent into the passenger or luggage compartments, or to any enclosed or semi-enclosed spaces within the vehicle that contains unprotected ignition sources."

*Paragraph 7.1.5., amend to read:*

"7.1.5. Fuel system leakage

The hydrogen fuelling line downstream of the main shut-off valve(s) to the fuel cell system or the engine shall not leak. Compliance shall be verified at NWP (Annex 5, paragraph 5. test procedure)."

*Paragraph 7.2., amend to read:*

"7.2. Post-crash fuel system integrity

The vehicle fuel system shall comply with the following requirements after the vehicle crash tests in accordance with the following UN Regulations by also applying the test procedures prescribed in Annex 5 to this UN Regulation.

- (a) Frontal impact test procedures in accordance with UN Regulation No. 94, Annex 3 and UN Regulation No. 137, Annex 3 only to the extent where the UN Regulations apply as prescribed in their scope; and
- (b) Lateral impact test procedures in accordance with UN Regulation No. 95, Annex 4.

At the request of the manufacturer, for vehicles not in the scope of these UN Regulations and that are derived from M<sub>1</sub> or N<sub>1</sub> vehicle categories they may be tested in accordance with the crash test procedures in these UN Regulations.

This requirement is deemed to be met if the vehicle equipped with CHSS is approved in accordance with UN Regulation No. 94 (05 series of amendments or later) or UN Regulation No. 137 (03 series of amendments or later) for frontal impact and UN Regulation No. 95 (06 series of amendments or later) for lateral impact, as applicable in the scope of aforementioned crash regulations.

In case that one or more directions of the vehicle crash tests specified above are not applicable to the vehicle, the CHSS shall, instead, be subject to the relevant alternative accelerations in compliance with the acceleration corridors which are specified in Tables 3 to 5 in both positive and negative directions. CHSS shall comply with the relevant requirements in paragraphs 7.2.3. and 7.2.4. The accelerations shall be measured at the location where the CHSS is installed. The CHSS shall be mounted and fixed on the representative part of the vehicle. The mass used shall be representative for a fully equipped and filled CHSS.

The test pulse shall be within the minimum and maximum value as specified in Tables 3 to 5. A higher shock level and /or longer duration as described in the maximum value in Tables 3 to 5 can be applied to the CHSS if recommended by the manufacturer.

Figure 3  
Generic description of test pulses

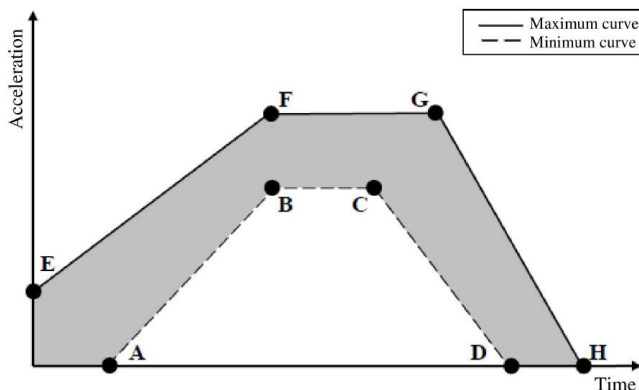


Table 3  
for M<sub>1</sub> and N<sub>1</sub> vehicles:

Point	Time (ms)	Acceleration (g)	
		Longitudinal	Transverse
A	20	0	0
B	50	20	8
C	65	20	8
D	100	0	0

E	0	10	4.5
F	50	28	15
G	80	28	15
H	120	0	0

Table 4  
for M<sub>2</sub> and N<sub>2</sub> vehicles:

Point	Time (ms)	Acceleration (g)	
		Longitudinal	Transverse
A	20	0	0
B	50	10	5
C	65	10	5
D	100	0	0
E	0	5	2.5
F	50	17	10
G	80	17	10
H	120	0	0

Table 5  
for M<sub>3</sub> and N<sub>3</sub> vehicles:

Point	Time (ms)	Acceleration (g)	
		Longitudinal	Transverse
A	20	0	0
B	50	6,6	5
C	65	6,6	5
D	100	0	0
E	0	4	2.5
F	50	12	10
G	80	12	10
H	120	0	0

A calculation method may be used instead of practical acceleration testing if its equivalence can be demonstrated by the manufacturer to the satisfaction of the Technical Service and in agreement with the Type Approval Authority."

Paragraph 7.2.3., amend to read:

"7.2.3. Container Displacement

The container(s) shall remain attached to the vehicle at a minimum of one attachment point."

*Paragraphs 7.2.4.1. to 7.2.4.2., amend to read:*

"7.2.4.1. Requirements on installation of the hydrogen storage system not subject to the frontal impact test:

The CHSS shall be mounted so that its primary closure devices are located in a position which is rearward of a vertical plane perpendicular to the centre line of the vehicle and located 420 mm rearward from the front edge of the vehicle. In any case the container should never be the outermost part of the vehicle.

7.2.4.2. Requirements on installation of the hydrogen storage system not subject to the lateral impact test:

The CHSS shall be mounted so that its primary closure devices are located in a position which is between the two vertical planes parallel to the centre line of the vehicle located 200 mm inside from the both outermost edges of the vehicle in the proximity of its container(s). In any case the container should never be the outermost part of the vehicle."

*Paragraph 7.2.4.3., amend to read:*

"7.2.4.3. Lateral impact test on compressed hydrogen storage system as alternative to 7.2.4.2.

At the request of the manufacturer, the CHSS may be tested in accordance with the applicable procedure specified in either (a) or (b) below, as alternative to the requirement of paragraph 7.2.4.2.

- (a) For CHSS installed with the lowest point of any primary closure devices located at a height equal to or less than 800 mm from the ground: Annex 8, Part 1;
- (b) For CHSS with the lowest point of any primary closure devices located at a height 800 mm above the ground: Annex 8, Part 2.

After this lateral impact test, the CHSS shall comply with the requirements in 7.2.1. and 7.2.3.

The CHSS to be tested will be decided by the manufacturer in agreement with the Technical Service.

A calculation method may be used instead of practical testing if its equivalence can be demonstrated by the applicant for approval to the satisfaction of the Technical Service and in agreement with the type-approval authority."

*Paragraphs 7.2.4.3.1. to 7.2.4.3.4., shall be deleted.*

*Paragraphs 9. to 9.3.2.3.7., amend to read:*

## **"9. Conformity of production**

9.1. Procedures concerning conformity of production shall conform to the general provisions defined in Schedule 1 to the Agreement (E/ECE/324-E/ECE/TRANS/505/Rev.3 and amend.1).

9.2. The production control of the compressed hydrogen storage system container shall satisfy the following additional requirements;

9.2.1. Every container or, upon agreement of the Type Approval Authority, every pressure bearing chamber of CHSS shall be pressurized smoothly and continually with a hydraulic fluid or gas to the target pressure of  $\geq 125$  per cent NWP until the target test pressure level is reached and then held for  $\geq 30$  seconds. Temperature variation during the test shall be taken into account. The quality variability of the products shall be assessed with a method defined by the manufacturer e.g., variability of elastic expansion, etc.

9.2.2. Sampling test

- 9.2.2.1. The sampling test and production control shall be implemented based on the batch of products. The maximum size of the batch shall not exceed 200 units or one shift of successive production, whichever is greater. The manufacturer shall conduct the tests specified in paragraph 9.2.3. on at least one CHSS randomly sampled from each batch of CHSS produced. In case that any defects are confirmed through the sampling tests, the manufacturer shall prevent the use of all CHSS in the same batch.
- 9.2.2.2. Upon request by the manufacturer after completion of at least 20 sequential batches, including at least 2,000 finished containers, complying with the requirements of paragraph 9.2.2.1., the type approval authority may recognise alternative procedures for sampling CHSS from its production, In this case, appropriate measures to trace the quality control data, that are sufficient to monitor the production variances due to different factors e.g., material, process, environments, for each CHSS produced shall be implemented. The manufacturer shall conduct the tests specified in paragraph 9.2.3. on CHSS randomly sampled according to the sampling rate determined by the manufacturer. In case that any defects are confirmed through the sampling tests, the manufacturer shall identify all the CHSS potentially having the same defects and take the appropriate measures to prevent further use of such CHSS.
- The sampling rate determined by the manufacturer shall be based on logical justifications and verified as a part of initial assessment in accordance with paragraph 9.1. Such sampling rate may include a strategy to adapt the sampling rate according to the factors influencing the stability of the product quality.
- 9.2.3. Procedure for sampling tests
- 9.2.3.1. Burst test
- The test shall be performed according to Annex 3, paragraph 2.1. (burst test). The burst pressure of each sample tested shall be at least BP<sub>min</sub> and the average burst pressure recorded of the last ten tests shall be at or above BP<sub>o</sub> - 10 per cent.
- 9.2.3.2. Ambient temperature pressure cycling test in batch testing
- The test shall be performed according to paragraph 2.2. (a) to (c) (hydrostatic pressure cycling test) of Annex 3, except that the temperature requirements for the fuelling fluid and the container skin, and the relative humidity requirement, do not apply. The container of the CHSS shall be pressure cycled using hydrostatic pressures  $\geq$  125 per cent of NWP, to 22,000 cycles in case of no leakage or until leakage occurs. The container of the CHSS shall not leak or burst within the first 11,000 cycles.

*Paragraph 13.1., amend to read:*

- "13.1. As from the official date of entry into force of the 02 series of amendments, no Contracting Party applying this UN Regulation shall refuse to grant or refuse to accept UN type approvals under this UN Regulation as amended by the 02 series of amendments."

*Paragraph 13.6., amend to read:*

- "13.6. As from 1 September 2027, Contracting Parties applying this Regulation shall not be obliged to accept type approvals to the preceding series of amendments, first issued after 1 September 2027. "

*Insert new paragraphs 13.7. to 13.9., to read:*

- "13.7. Contracting Parties applying this UN Regulation shall continue to accept type approvals issued according to any of the preceding series of amendments to this Regulation first issued before 1 September 2027, provided the transitional provisions in these respective previous series of amendments foresee this possibility.

- 13.8. Contracting Parties applying this UN Regulation may grant type approvals according to any preceding series of amendments to this UN Regulation.
- 13.9. Contracting Parties applying this UN Regulation shall continue to grant extensions of existing approvals to any preceding series of amendments to this UN Regulation."

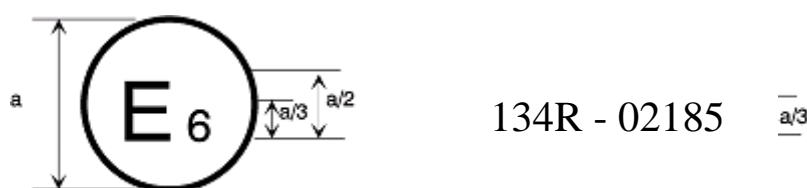
Annex 2., amend to read:

## "Annex 2

### Arrangements of the approval marks

Model A

(See paragraphs 4.4. to 4.4.2. of this Regulation)

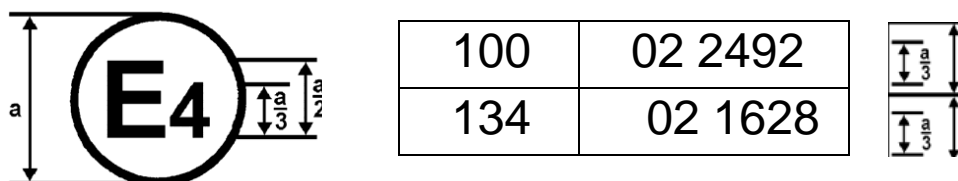


a = 8 mm min

The above approval mark affixed to a vehicle/ storage system/specific component shows that the vehicle/storage system/specific component type concerned has been approved in Belgium (E 6) for its the safety-related performance of hydrogen-fuelled vehicles pursuant to Regulation No. 134. The first two digits of the approval number indicate that the approval already contained the 02 series of amendments at the time of approval.

Model B

(See paragraph 4.5. of this Regulation)



a = 8 mm min.

The above approval mark affixed to a vehicle shows that the road vehicle concerned has been approved in the Netherlands (E 4) pursuant to Regulations Nos. 134 and 100.\* The approval number indicates that, at the dates when the respective approvals were granted, Regulation No. 100 was amended by the 02 series of amendments and Regulation No. 134 was amended by the 02 series of amendments. "

\* The latter number is given only as an example.

*Annex 3 (all paragraphs), amend to read:*

## "Annex 3

### **Test procedures for the compressed hydrogen storage system**

1. Test procedures for qualification requirements of CHSS are organized as follows:

Paragraphs 2. and 3. of this Annex contains the test procedures for baseline performance metrics (requirement of paragraph 5.1. of this UN Regulation) and performance durability (requirement of paragraph 5.2. of this UN Regulation)

Paragraph 4 of this Annex contains the test procedures for expected on-road performance (requirement of paragraph 5.3. of this UN Regulation)

Paragraph 5 of this Annex contains the test procedures for service terminating performance in fire (requirement of paragraph 5.4. of this UN Regulation)

Unless otherwise specified, the ambient temperature for all tests shall be  $20 \pm 15^{\circ}\text{C}$ .

Unless otherwise specified data sampling for pressure cycling shall be at least 1 Hz.

Unless otherwise specified, the acceptable tolerances of the open ended test parameters may be recommended by the manufacturer.

2. Test procedures for baseline performance metrics

- 2.1. Burst test (hydraulic)

The burst test is conducted at the ambient temperature using a hydraulic fluid. The rate of pressurization is less than or equal to 1.4 MPa/sec for pressures higher than 150 per cent of the nominal working pressure. If the rate exceeds 0.35 MPa/sec at pressures higher than 150 per cent NWP, then either the container is placed in series between the pressure source and the pressure measurement device, or the time at the pressure above a target burst pressure exceeds 5 seconds. The burst pressure of the container shall be recorded.

- 2.2. Ambient pressure cycling test (hydraulic)

The test is performed in accordance with the following procedure and the test parameters specified in Table 1 below:

- (a) The test article is filled with a hydraulic fluid;
- (b) The test article and fluid are stabilized at the temperature specified in Table 1 at the start of testing. The environment, hydraulic fluid and the surface of the test article are maintained at the specified temperature for the duration of the cycling. The test article temperature may vary from the environmental temperature during cycling;
- (c) The test article is pressure cycled between  $2 \pm 1$  MPa and the target pressures specified in accordance with Table 1;
- (d) The temperature of the hydraulic fluid entering the container shall be maintained at the specified temperature and monitored as close as possible to the container inlet;

Note: The manufacturer may specify a hydraulic pressure cycle profile that will prevent premature failure of the container due to test conditions outside of the container design envelope.



Table 1  
**Pressure cycles and conditions**

<i>Purpose</i>	<i>Number of cycles</i>	<i>Target Pressure</i>	<i>Temperature</i>	<i>Rate</i>
Baseline initial pressure cycle life (paragraph 5.1.2.)	22,000 or until leak occurs	≥ 125 per cent NWP	Environment: 20 ± 15 °C Hydraulic fluid: 20 ± 15 °C	≤ 10 cycles per minute

3. Test procedures for performance durability (requirement of paragraph 5.2. of this Regulation)

3.1. Proof pressure test

The container with its container attachments (if any), as specified, is pressurized smoothly and continually with a hydraulic fluid or gas until the target test pressure level is reached and then held for the duration specified in Table 2 below:

Table 2  
**Target pressure and holding duration of proof pressure test**

<i>Purpose</i>	<i>Target pressure</i>	<i>Holding duration</i>
(Initial) proof pressure test (paragraph 5.2.1. and 5.3.1.)	≥ 150 per cent NWP	≥ 30 seconds
Residual proof pressure test (paragraph 5.2.7. and 5.3.4.)	≥ 180 per cent NWP	≥ 4 minutes

3.2. Drop (impact) test (unpressurized)

The container and its container attachments (if any) is drop tested without internal pressurization or attached valves. The surface onto which the test article is dropped shall be a smooth, horizontal concrete pad or other flooring type with equivalent hardness. No attempt shall be made to prevent the test article from bouncing or falling over during a drop test, but the test article shall be prevented from falling over during the vertical drop test.

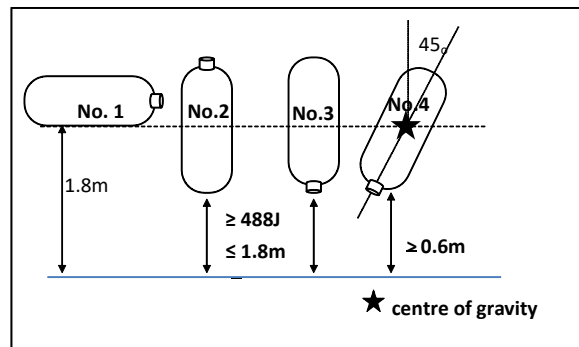
The test article shall be dropped in any one of the following four orientations:

- (i) From a horizontal position with the bottom 1.8 m above the surface onto which it is dropped. In case of non-axisymmetric container, the largest projection area of the container shall be oriented downward and aligned horizontally, the shut-off valve interface location and its centre of gravity should be horizontally aligned as it is feasible;
- (ii) From a vertical position with the shut-off valve interface location upward, with a drop height calculated based on a potential energy of 488 J. In no case shall the height of the lower end be less than 0.1m or greater than 1.8m. In case of non-axisymmetric container, the shut-off valve interface location and its centre of gravity shall be vertically aligned;
- (iii) From a vertical position with the shut-off valve interface location downward, with a drop height calculated based on a potential energy of 488 J. In no case shall the height of the lower end be less than 0.1m or greater than 1.8m. If the container is symmetrical (identical ends), this drop orientation is not required. In case of non-axisymmetric container, the shut-off valve interface location and its centre of gravity shall be vertically aligned;

- (iv) From a 45° angle from the vertical orientation with the shut-off valve interface location downward with its centre of gravity at 1.8 m above the ground. However, if the bottom is closer to the ground than 0.6 m, the drop angle shall be changed to maintain a minimum height of 0.6 m and a centre of gravity at 1.8 m above the ground. In case of non-axisymmetric container, the line passing the shut-off valve interface location end and its centre of gravity shall be 45° angled from vertical orientation and the shut-off valve interface location shall become the lowest.

The four drop orientations are illustrated in Figure 1.

Figure 1  
Drop orientations



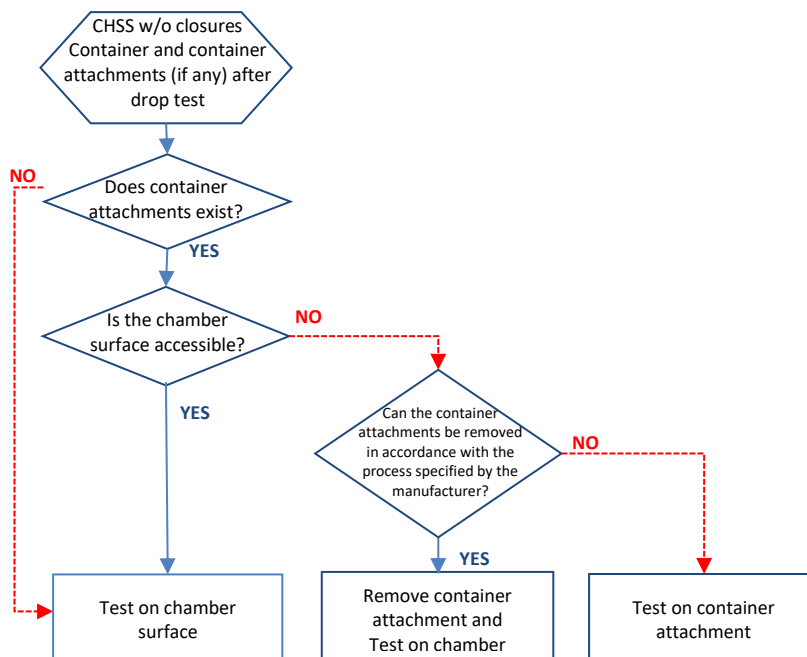
### 3.3. Surface damage test (unpressurized)

The surface damage tests and the chemical exposure tests (Annex 3, paragraph 3.4.) shall be conducted on the surface of the pressure bearing chamber of the container as long as it is accessible regardless of the existence of the container attachments.

If the container attachments can be removed in accordance with the process specified by the manufacturer, then the container attachments shall be removed, and the tests shall be conducted on the surface of the pressure bearing chamber of the container.

Otherwise, the tests shall be conducted on the surface of the container attachments as indicated in Figure 2.

Figure 2  
Surface damage flow chart



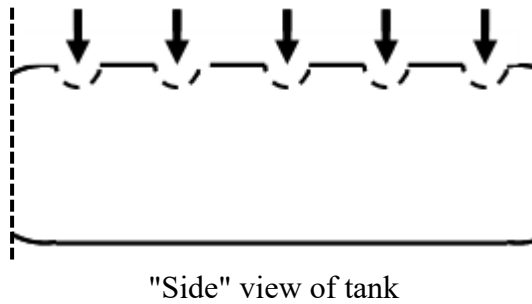
The test proceeds in the following sequence:

- (a) Surface flaw generation: A saw cut at least 0.75mm deep and 200mm long is made on the surface specified above.

If the container is to be affixed to the vehicle by compressing its composite surface, then a second cut at least 1.25 mm deep and 25 mm long is applied at the end of the container which is opposite to the location of the first cut;

- (b) Pendulum impacts: A surface of the test article opposite to the surface specified above or a surface of a different chamber, in the case of a container with multiple permanently interconnected chambers, is divided into five distinct (not overlapping) areas 100 mm in diameter each (see Figure 3). Immediately following a minimum of 12 hours preconditioning at  $\leq -40$  °C in an environmental chamber, the centre of each of the five areas sustains the impact of a pendulum having a pyramid with equilateral faces and square base, the summit and edges being rounded to a radius of 3 mm. The centre of impact of the pendulum coincides with the centre of gravity of the pyramid. The energy of the pendulum at the moment of impact with each of the five marked areas on the container is  $\geq 30$  J. The test article is secured in place during pendulum impacts and not under pressure.

Figure 3  
Side view of container



#### 3.4. Chemical exposure and ambient-temperature pressure cycling test

Each of the 5 areas of the unpressurized container (with container attachments, if applicable) preconditioned by pendulum impact (Annex 3, paragraph 3.3.) is exposed to one of five solutions:

- (a) 19 per cent (by volume) sulphuric acid in water (battery acid);
- (b) 25 per cent (by weight) sodium hydroxide in water;
- (c) 5 per cent (by volume) methanol in gasoline (fluids in fuelling stations);
- (d) 28 per cent (by weight) ammonium nitrate in water (urea solution); and
- (e) 50 per cent (by volume) methyl alcohol in water (windshield washer fluid).

The test article is oriented with the fluid exposure areas on top. A pad of glass wool approximately 0.5 mm thick and 100 mm in diameter is placed on each of the five preconditioned areas. A sufficient amount of the test fluid is applied to the glass wool sufficient to ensure that the pad is wetted across its surface and through its thickness for the duration of the test. A plastic covering may be applied over the glass wool to prevent evaporation.

The exposure of the test article with the glass wool is maintained for at least 48 hours with the test article held at  $\geq 125$  per cent NWP (applied hydraulically) and ambient temperature before the test article is subjected to further testing.

The test article is pressure cycled from  $2 \pm 1$  MPa to the target pressures specified in Table 3. The glass wool pads are removed and the container surface is rinsed with water after the pressure cycling is completed.

Table 3  
**Pressure cycles and conditions - chemical exposure and ambient temperature pressure cycling test**

<i>Purpose</i>	<i>Number of cycles</i>	<i>Target Pressure</i>	<i>Temperature</i>	<i>Rate</i>
Chemical exposure and ambient temperature pressure cycling test (paragraph 5.2.4.)	60 per cent the specified number of cycles determined in paragraph 5.1.2.	≥ 125 per cent NWP	Environment: 20 ± 15 °C Hydraulic fluid: 20 ± 15 °C	≤ 10 cycles per minute
	of which the last 10 cycles	≥ 150 per cent NWP		

3.5. Static pressure test (hydraulic)

The test article is filled with a hydraulic fluid and pressurized to ≥ 125 per cent NWP in a temperature-controlled chamber at ≥ 85 °C for at least 1,000 hr during which the temperature of the chamber and the surface of the test article are maintained at the target temperature for the specified duration.

3.6. Extreme temperature pressure cycling test

The test is performed in accordance with the following procedure and the test parameters specified in Table 4:

- (a) The test article is filled with a hydraulic fluid for each test;
- (b) The test article and fluid are stabilized at the temperature and relative humidity specified in Table 4 at the start of each test. The environment, hydraulic fluid and the surface of the test article are maintained at the specified temperature for the duration of the cycling. The test article temperature may vary from the environmental temperature during cycling;
- (c) The test article is pressure cycled from  $2 \pm 1$  MPa to the target pressures specified in Table 4;
- (d) The temperature of the hydraulic fluid entering the container shall be maintained at the specified temperature and monitored as close as possible to the container inlet.

Note: It is recommended that the container is kept at greater than atmospheric pressure for the duration of the testing and is only depressurized once stabilized to ambient temperature.

Table 4  
**Pressure cycles and conditions - extreme temperature pressure cycling test**

<i>Purpose</i>	<i>Number of cycles</i>	<i>Target Pressure</i>	<i>Temperature</i>	<i>Rate</i>
Extreme cold test	20 per cent the specified number of cycles determined in paragraph 5.1.1.2.	≥ 80 per cent NWP	Environment: ≤ -40 °C at the start of each test Hydraulic fluid and surface: ≤ -40 °C for duration of the cycling	≤ 10 cycles per minute
Extreme hot test	20 per cent the specified number of cycles determined in paragraph 5.1.1.2.	≥ 125 per cent NWP	Environment: ≥ 85 °C and ≥ 80 per cent relative humidity Hydraulic fluid & surface: ≥ 85 °C for duration of the cycling	≤ 10 cycles per minute

4. Test procedures for expected on-road performance (paragraph 5.3. of this Regulation)

Test sequence and parameters of the ambient and extreme temperature gas pressure cycling test are specified in Tables 5a and 5b.

Table 5a  
**Ambient and extreme temperature gas pressure cycling test parameters**

<i>No. of cycles</i>	<i>Ambient Conditions</i>	<i>Initial CHSS Equilibration</i>	<i>Fuel Delivery Temperature</i>	<i>Initial Pressure</i>	<i>Target Pressure</i>
5	≤ -25°C	≤ -25°C	20 ± 5°C	≤ 2 MPa	≥ 100 per cent SOC
5	≤ -25°C	≤ -25°C	-33°C to -40°C	≤ 2 MPa	≥ 100 per cent SOC
15	≤ -25°C	N/A	-33°C to -40°C	≤ 2 MPa	≥ 100 per cent SOC
5	≥ 50°C, ≥ 80 per cent RH	≥ 50°C, ≥ 80 per cent RH	-33°C to -40°C	≤ 2 MPa	≥ 100 per cent SOC
20	≥ 50°C, ≥ 80 per cent RH	N/A	-33°C to -40°C	≤ 2 MPa	≥ 100 per cent SOC
200	20°C ± 5°C	N/A	-33°C to -40°C	≤ 2 MPa	≥ 100 per cent SOC
1st permeation	55°C to 60°C	55°C to 60°C	N/A	N/A	≥ 100 per cent SOC
25	≥ 50°C, ≥ 80 per cent RH	N/A	-33°C to -40°C	≤ 2 MPa	≥ 100 per cent SOC
25	≤ -25°C	N/A	-33°C to -40°C	≤ 2 MPa	≥ 100 per cent SOC
200	20 ± 5°C	N/A	-33°C to -40°C	≤ 2 MPa	≥ 100 per cent SOC
2nd permeation	55°C to 60°C	55°C to 60°C	N/A	N/A	≥ 100 per cent SOC

Table 5b  
**CHSS pressurization rates for ambient and extreme temperature gas pressure cycling tests**

CHSS volume (L)	CHSS Pressurization Rate (MPa/min)			
	50 °C Ambient $-40\text{ °C} \leq T_{\text{fuel}} \leq -33\text{ °C}$	20 °C Ambient $-40\text{ °C} \leq T_{\text{fuel}} \leq -33\text{ °C}$	-25 °C Ambient $-40\text{ °C} \leq T_{\text{fuel}} \leq -33\text{ °C}$	-25 °C Ambient $T_{\text{fuel}} = 20\text{ °C} \pm 5\text{ °C}$
50	7.6	19.9	28.5	13.1
100	7.6	19.9	28.5	7.7
174	7.6	19.9	19.9	5.2
250	7.6	19.9	19.9	4.1
300	7.6	16.5	16.5	3.6
400	7.6	12.4	12.4	2.9
500	7.6	9.9	9.9	2.3
600	7.6	8.3	8.3	2.1
700	7.1	7.1	7.1	1.9
1 000	5.0	5.0	5.0	1.4
1 500	3.3	3.3	3.3	1.0
2 000	2.5	2.5	2.5	0.7
2 500	2.0	2.0	2.0	0.5

4.1. Gas pressure cycling test (pneumatic)

- (a) The CHSS is pressure cycled using hydrogen gas for total 500 cycles, which are divided into two groups of 250 cycles each according to the test parameters specified in Table 5a;

The specified temperature and relative humidity is maintained within the test environment throughout each pressure cycle. When required in the test specification, the CHSS temperature is stabilized at the external environmental temperature between pressure cycles. If system controls that are active during vehicle service prevent the pressure from dropping below a specified pressure, the test cycles shall not go below that specified pressure;

The fuel delivery temperature shall conform to the specified range within 30 seconds of fuelling initiation;

- (b) The ramp rate for pressurization shall be greater than or equal to the linearly interpolated rate in Table 5b according to the CHSS volume; however, if the measured internal temperature in the CHSS container is greater than 85°C, then the pressure ramp rate shall be decreased;
- (c) If devices and/or controls are used in the intended vehicle application to prevent an extreme internal temperature of the CHSS container, the test may be conducted with these devices and/or controls (or equivalent measures);
- (d) The de-fuelling rate shall be greater than or equal to the intended vehicle's maximum fuel-demand rate. Out of the 500 pressure cycles, any fifty pressure cycles are performed using a de-fuelling rate greater than or equal to the maintenance de-fuelling rate specified by the manufacturer on CHSS container labelling or operating/maintenance manuals;

- (e) The maximum allowable leak rate from the CHSS from a single point is in accordance with Annex 3, paragraph 4.3(b).

4.2. Gas permeation test (pneumatic)

This test is performed after each group of 250 pneumatic pressure cycles conducted in accordance with Table 5a in Annex 3, paragraph 4.

The CHSS is fully filled with hydrogen gas to  $\geq 100$  per cent SOC and soaked for a minimum of 12 hours at 55 °C to 60 °C in a sealed chamber prior to the start of the test. The test shall continue until the permeation rate reaches a steady state based on at least 3 consecutive rates separated by at least 12 hours being within  $\pm 10$  per cent of the previous rate, or 500 hours, whichever occurs first.

4.3. Localized gas leak test (pneumatic)

A bubble test may be used to fulfil this requirement. The following procedure is used when conducting the bubble test:

- (a) The exhaust of the shut-off valve (and other internal connections to hydrogen systems) shall be capped for this test (as the test is focused on external leakage).

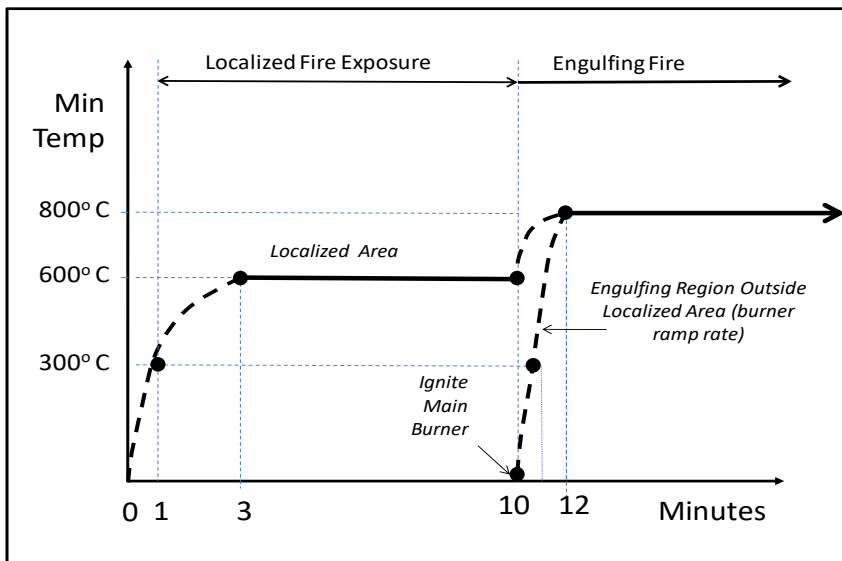
At the discretion of the Technical Service, the test article may be immersed in the leak-test fluid or leak-test fluid applied to the test article when resting in open air. Bubbles can vary greatly in size, depending on conditions. The tester estimates the gas leakage based on the size and rate of bubble formation.

- (b) For a localized rate of 0.005 mg/sec (3.6 Nml/min), the resultant allowable rate of bubble generation is about 2,030 bubbles per minute for a typical bubble size of 1.5 mm in diameter. Even if much larger bubbles are formed, the leak shall be readily detectable. For an unusually large bubble size of 6 mm in diameter, the allowable bubble rate would be approximately 32 bubbles per minute.

5. Test procedures for two-stage localized/engulfing fire test (paragraph 5.4. of this UN Regulation)

The test consists of two stages: a localized fire stage followed by an engulfing stage as described in Figure 4.

Figure 4  
Temperature profile of fire test





The CHSS test article to be evaluated is defined in Annex 3, paragraph 5.1.

Test conditions and wind shielding requirements for conducting the fire test are defined in Annex 3, paragraph 5.2.

The fuel supply and burner for the fire test are defined in Annex 3, paragraph 5.3.

A pre-test checkout of the burner is defined in Annex 3, paragraph 5.4. to ensure that the burner is operating within the established thermal criteria prior to the CHSS fire test. This test is required when the conditions set forth in Annex 3, paragraph 5.4.1. indicate that the pre-test checkout is appropriate.

Final preparations for the CHSS fire test are defined in Annex 3, paragraphs 5.5 and 5.6, and the test procedure for the CHSS fire test under two-stage localized/engulfing fire test is defined in Annex 3, paragraph 5.7.

#### 5.1. CHSS test article

In addition to the container and primary closure devices such as shut-off valve(s), check valve(s), and TPRD(s) required to isolate the system, the CHSS test article shall include container attachments (if any) including gas housings or barriers that could impede TPRD response. Vent lines shall be connected to TPRDs to direct TPRD exhausts in a manner representative of the configuration in the vehicle.

At the option of the manufacturer, the CHSS test article may include vehicle-specific structural framing, shields and panels, and/or other protective features intended to protect the CHSS from fire exposures consistent with the fire threats on the CHSS as installed in the specific vehicle.

#### 5.2. Test conditions and wind shielding

Testing can be conducted either indoors or outdoors.

Ambient temperature and wind speed and direction shall be measured and recorded if testing conducted outdoors.

Outdoor testing shall not be conducted when precipitation (i.e., rain, snow, sleet, etc.) is occurring unless the test area with the test article and burner is protected such that the precipitation does not adversely affect the test result.

Wind shielding such as are walls, fencing, and/or enclosures shall be used for the fire tests at sites susceptible to wind effects during the tests (pre-test checkout and CHSS fire test). The wind shielding shall provide at least 0.5 m separation between the CHSS test article (or pre-test cylinder) and the wind shields such that the fire can freely draft and that the length of jet flames (if any) from the CHSS test article can be confirmed. Openings (or other provisions) shall be provided in wind shielding to allow fresh air to enter the test area and for the combustion products to be exhausted. The adequacy of wind shielding shall be verified by compliance to Table 10 during a pre-test check-out prior to the CHSS fire test.

**NOTE:** Rupture of container during the fire test is likely to result in blast waves and the rapid expulsion of container materials and attachments as well as the hydrogen contents.

These effects can result in uncontrolled movement of the CHSS test article and secondary explosions due to the build-up of high pressure, flammable gas mixtures within the test area and wind shielding (if used).

Countermeasures to these effects need to be addressed and implemented as part of locating the test site relative to other equipment and designing and constructing wind shielding (if used) and test support structure to prevent severe injury to personnel and unacceptable property damage.

### 5.3. Burner definition

In order to conduct the two-stage localized/engulfing fire test, the burner is divided into two zones:

- (a) The localized burner zone operates by itself during the localized fire stage.
- (b) The engulfing burner extension simulates the spread of the fire from the localized burner zone to the remainder of the burner. The engulfing burner zone is comprised of both the localized burner zone and the engulfing fire extension.

#### 5.3.1. Fuel supply and burner control

The localized and engulfing burners shall be LPG-fired.

The LPG burner fuel flow to both the localized burner zone and engulfing burner extension shall be measured to set burner fuel flows to the specific heat release rates (HRR/As) defined in Annex 3, paragraph 5.4.5.

The measured fuel flow(s) shall be recorded throughout the test on a 1-second basis.

#### 5.3.2. Burner configuration

##### 5.3.2.1. The length of the localized burner zone ( $L_{LOC}$ ) is $250 \pm 50$ mm.

The length of the engulfing burner extension ( $L_{EXT}$ ) shall be a maximum of  $1,400 \pm 50$  mm. A burner with the specified maximum extension can be used for all fire tests. Engulfing burner extensions shorter than the maximum are acceptable as long the burner extends beyond of the CHSS test article when positioned for the CHSS fire test.

The total length of the engulfing burner zone ( $L_{ENG}$ ) is the sum  $L_{LOC}$  and  $L_{EXT}$ . The maximum value is  $1,650 \pm 100$  mm based on the specifications above.

The width ( $W$ ) of both the localized and engulfing burner zones shall be  $500 \pm 50$  mm regardless of container width/ diameter.

The burner nozzle configuration and installation on the manifolds (or "rails") shall be consistent with Table 6. The number of nozzles ( $N_{LOC}$  and  $N_{EXT}$ ) on the rails of the localized burner zone and the engulfing burner extension and the nozzle spacing ( $S_N$ ) shall be selected such that the resultant lengths of the localized burner zone and the engulfing burner extension ( $L_{LOC}$  and  $L_{EXT}$ ) meet requirements defined above. Similarly, the number of rails ( $N_R$ ) and rail spacing ( $S_R$ ) shall be selected such that the width of the burners meets requirements defined above.

#### NOTES:

- (a) The resultant lengths of the localized burner zone and the engulfing burner extension are determined by;

$$L_{LOC} = N_{LOC} \times S_N$$

and

$$L_{EXT} = N_{EXT} \times S_N$$

based on selected values for the number of nozzles ( $N_{LOC}$  and  $N_{EXT}$  in the localized burner zone and the engulfing burner extension, respectively) and the nozzle spacing ( $S_N$ ).

Similarly, the resultant width ( $W$ ) of the burners is determined by;

$$W = (N_R - 1) \times S_R$$

based on selected values for number of rails ( $N_R$ ) and rail spacing ( $S_R$ ).

- (b) As illustrated in Figure 7 below, the nozzles on the third and fourth rails aim toward the centre of the burner to form a "hot zone" in this targeted area.

**Table 6**  
**Definition of burner nozzles for the prescribed burner**

<i>Item</i>	<i>Description</i>
Nozzle type	LPG fuel nozzle with air pre-mix
- LPG orifice in nozzle	1.0 ± 0.1 mm ID
- Air ports in nozzle	Four (4) holes, 6.4 mm ± 0.6 mm ID
- Fuel/Air mixing tube in nozzle	10 ± 1 mm ID
Number of rails	6
Centre-to-centre spacing of rails	100 ± 10 mm
Centre-to-centre nozzle spacing along the rails	50 ± 5 mm

5.3.2.2. The values for  $L_{LOC}$ ,  $L_{EXT}$ , and  $W$  defined above shall be used for calculating HRR/As for the localized burner zone and engulfing burner extension.

The borders of the localized burner zone and the engulfing burner extension shall be defined using  $L_{LOC}$ ,  $L_{EXT}$ , and  $W$  so that test articles can be properly located and oriented for CHSS fire test. The borderline between the localized burner zone and the engulfing burner extension is located mid-way between the nozzles of the two zones and used as a datum for locating the outside borders at distances  $L_{LOC}$  and  $L_{EXT}$  away from the datum towards the localized burner zone and the engulfing burner extension, respectively. The centres of the outside rails of the burner zone(s) define the remaining two borders.

5.4. Pre-test checkout of burner

The purpose of the pre-test checkout is to verify that the localized and engulfing burner zones are operating as expected and that the test setup including wind shields are functional and capable of delivering repeatable results prior to conducting the CHSS fire tests.

5.4.1. Pre-test checkout frequency

This pre-test shall be performed at least once prior to conducting CHSS fire tests. If the burner and test setup is modified, then the pre-test shall be repeated before CHSS fire test.

5.4.2. Pre-test cylinder definition

A 320 mm diameter pre-test cylinder (fabricated from 300 mm/12 inch Schedule 40 NPS steel pipe with end caps) similar to vehicle fire tests shall be used for the burner pre-test.

The cylindrical length of the pre-test cylinder shall be at least 800mm, and the overall length shall be equal or longer than the CHSS test article (up to maximum engulfing burner length in Annex 3, paragraph 5.1.1.).

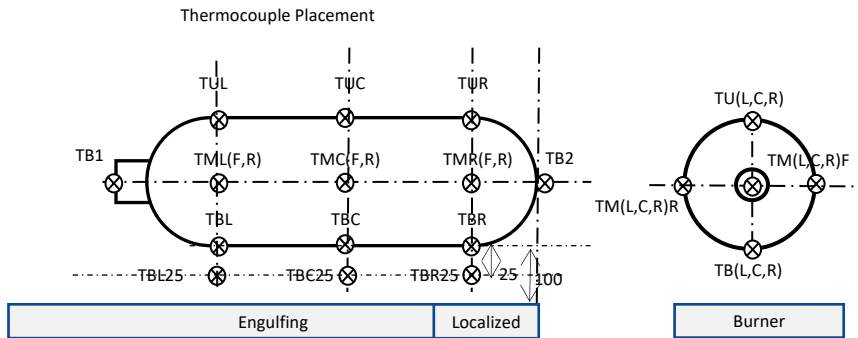
5.4.3. Instrumentation and data processing for pre-test check-out

5.4.3.1. The pre-test cylinder shall be instrumented to ensure that the burner and test setup will produce temperature levels consistent with performance-based requirements of the localized and engulfing fire zones. The location of the instrumentation shall be adjusted along the cylindrical section of the pre-test cylinder to be consistent with the targeted localized and engulfing fire zones of the CHSS test article. One set of instrumentation on the cylindrical section shall be centrally located within the localized zone, and the other two sets spread out over the remaining length of the engulfing fire zone (outside the localized fire zone).

As an example of the process, Figure 5 illustrates a common situation where a container is protected by a TPRD on one end (i.e., the left end) so the localized fire zone is located on the right-end end. The surface temperatures are

measured on the top, middle, and bottom of the pre-test cylinder in three locations along the length of the cylinder. The location on the right end of the cylindrical section is centrally-located in the targeted localized zone, and the other two locations are in the centre and left ends of the targeted engulfing fire zones along the cylindrical section.

Figure 5  
Example of placement of instrumentation on the pre-test cylinder



Temperature measurements on the pre-test cylinder shall be performed by  $\phi 3.2$  mm (or less) K-type sheath thermocouples that are located within a 5 mm gap from the pipe surface that are held on the surface by straps or other mechanical attachments. Temperature measurements shown in Figure 5 are defined as follows:

- TBR, TBC, and TBL are temperature measurements on the bottom surface of the pre-test cylinder that are directly exposed to the burner flame.
- TMRF, TMCF, TMLF, TMRR, TMCR, and TMLR are temperature measurements on the surface of the pre-test cylinder at mid-height. These temperatures are used for data collection only during the pre-test verification and calibration of the localized and engulfing fires.
- TUR, TUC, and TUL are temperature measurements on the top surface of the pre-test cylinder that are opposite the side directly exposed to the burner flame.

Additional thermocouples may be located at TPRD sensing points or any other locations for optional diagnostic purposes.

- 5.4.3.2. Thermocouples shall also be located  $25 \pm 5$  mm below the pre-test cylinder along the length of the cylinder for the purpose of developing reference temperature levels during the pre-test checkout that can be subsequently used for monitoring the burner during the CHSS fire test. Three (3) thermocouples (TBR25, TBC25, and TBL25) shall correspond to pre-test cylinder instrumentation as shown in Figure 5. Thermocouples used to back up or supplement TBR25, TBC25, and TBL25 may also be added along the centre line of the burner. See paragraph 5.6. for requirements for positioning thermocouples for burner monitoring during the CHSS fire test.

The thermocouples used for burner monitoring shall be unshielded (i.e., unprotected by metal wells)  $\phi 3.2$  mm (or less) K-type sheath thermocouples. Given the need to maintain the distance from the steel container within  $\pm 5$  mm, these thermocouples shall be mechanically supported to prevent movement or drooping. If testing of CHSSs with large width/diameters is contemplated, then mounting shall maintain the distance between the CHSS and the burner monitors as the spacing between the burner and CHSS is adjusted in paragraph 5.4.5.5.

- 5.4.3.3. Thermocouple readings shall be recorded at least once a second and then used to calculate the following parameters:
- (a)  $TB_{LOC}$  is the bottom surface temperature of the pre-test cylinder based on TBR;
  - (b)  $TMF_{LOC}$  are the surface temperatures of the front side of the pre-test cylinder based on TMRF;
  - (c)  $TMR_{LOC}$  is the surface temperatures of the rear side of pre-test cylinder based on TMRR;
  - (d)  $TU_{LOC}$  is the top surface temperature of the pre-test cylinder based on TUR;
  - (e)  $TB_{LOC25}$  is the burner monitor below the pre-test cylinder (and subsequently below the CHSS test article in paragraph 5.6.) based on TBR25. Thermocouples used to back up or supplement TBR25 may also be included in the calculation of the average temperature of the burner monitors in the localized fire zone. Any thermocouple measurement that has been compromised or failed (or is not located within the localized fire zone) shall be disregarded from the calculation of average temperature of the burner monitor.
  - (f)  $TB_{ENG}$  is the bottom surface temperature of the pre-test cylinder based on the average of TBR, TBC, or TBL within the engulfing fire zone.
  - (g)  $TMF_{ENG}$  is the surface temperature of the front side of the pre-test cylinder based on the average of TMLF, TMCF, and TMRF within the engulfing fire zone.
  - (h)  $TMR_{ENG}$  is the surface temperatures of the rear side of the pre-test cylinder based on the average of TMLR, TMCR, and TMRR within the engulfing fire zone.
  - (i)  $TU_{ENG}$  is the top surface temperature of the pre-test cylinder based on the average of TUR, TUC, or TUL within the engulfing fire zone.
  - (j)  $TB_{ENG25}$  is the burner monitor below the pre-test cylinder (and subsequently below the CHSS test article in paragraph 5.6.) based on the average of the three required thermocouples (TBR25, TBC25, or TBL25 for the pre-test checkout) within the engulfing fire zone. Thermocouples used to back up or supplement TBR25, TBC25, or TBL25 may also be included in the calculation of average temperature of the burner monitor in the engulfing fire zone. Any thermocouple measurement that has been compromised or failed (or is not located within the engulfing fire zone) shall be disregarded from the calculation of average temperature in the engulfing fire zone.

5.4.4. Mounting of the pre-test cylinder

The pre-test cylinder used for the pre-test checkout shall be mounted at a height of  $100 \pm 5$  mm above the burner and located over the burner such that nozzles from the two centrally-located manifolds are pointing toward the bottom centre of the steel container.

NOTE: See the diagrams in Figure 6 and Figure 7 for examples of the mounting.

Figure 6  
**Description of instrumentation for the steel container used for pre-test checkout**

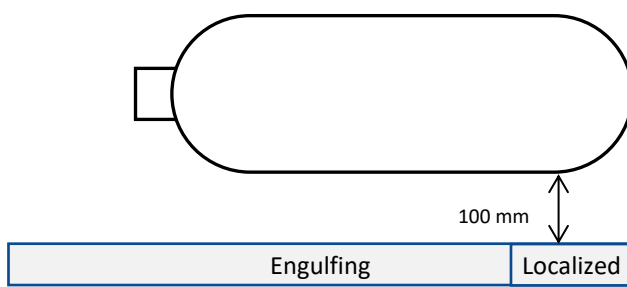
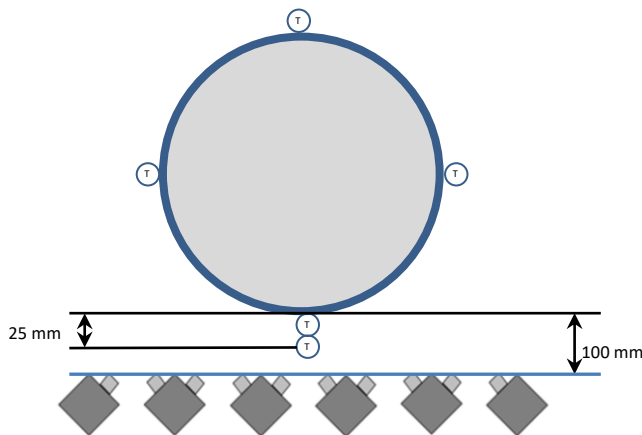


Figure 7  
**Position the bottom of the container relative to the burner**



- 5.4.5. Pre-test checkout process
  - 5.4.5.1. Prior to pre-test checkout of the burner, wind shieldings shall be installed in accordance with paragraph 5.2.
  - 5.4.5.2. The burner shall, at a minimum, be operated at fuel flow setpoints that match the settings intended for the localized and engulfing burners during the CHSS fire test. Suggested settings for the burners are provided in Table 7; however, any setting within the allowable ranges of HRR/A in Table 7 may be selected.

NOTE: During the engulfing fire stage, both the localized burner and the engulfing burner extension need to be set to the intended HRR/A for uniform heat release from the engulfing burner.

Table 7  
**Allowable range of operation and the suggested settings for the prescribed burner**

<i>Fire Stage</i>	<i>Allowable Range of Specific Heat Release Rate (HRR/A)</i>	<i>Suggested Setting of Specific Heat Release Rate (HRR/A)</i>
Localized Burner	200 - 500 kW/m <sup>2</sup>	300 kW/m <sup>2</sup>
Engulfing Burner	400 - 1000 kW/m <sup>2</sup>	700 kW/m <sup>2</sup>

- 5.4.5.3. The 60-second rolling averages of individual temperature readings in the localized fire zone (i.e.,  $T_{BLOC}$ ,  $T_{MFLOC}$ ,  $T_{MRLOC}$ , and  $T_{ULOC}$ ) and the engulfing fire zone (i.e.,  $T_{BR}$ ,  $T_{BC}$ ,  $T_{BL}$ ,  $T_{MRF}$ ,  $T_{MCF}$ ,  $T_{MLF}$ ,  $T_{MRR}$ ,  $T_{MCR}$ ,  $T_{MLR}$ ,  $T_{UR}$ ,  $T_{UC}$ , and  $T_{UL}$ ) shall be in accordance with Table 8 at the HRR/A settings selected for the CHSS fire test in paragraph 5.7.

Table 8  
**Criteria for acceptance of localized and engulfing burners using alternative burner configurations**

<i>Fire Stage</i>	<i>Allowable Temperature Range on Bottom of Pre-test cylinder</i>	<i>Allowable Temperature Range on Sides of Pre-test cylinder</i>	<i>Allowable Temperature Range on Top of Pre-test cylinder</i>
Localized Burner	$450\text{ °C} < T_{B_{LOC}} < 750\text{ °C}$	$T_{M_{F_{LOC}}} < 750\text{ °C}$ and $T_{M_{R_{LOC}}} < 750\text{ °C}$	$T_{U_{LOC}} < 300\text{ °C}$
Engulfing Burner	$T_{B_{ENG}} > 600\text{ °C}$		$T_{U_{ENG}} > 100\text{ °C}$ and $T_{U_{ENG}} < T_{B_{ENG}}$ when $T_{U_{ENG}} > 750\text{ °C}$

5.4.5.4. Additionally, the allowable limits for the burner monitors during subsequent CHSS fire test shall be established based on test results at the expected localized and engulfing burner settings during the pre-test checkout:

- (a) The minimum value for the burner monitor during the localized fire stage ( $T_{min_{LOC25}}$ ) shall be calculated by subtracting 50 °C from the 60-second rolling average of  $T_{B_{LOC25}}$ . If the resultant minimum values exceed 600 °C, the minimum value is set to 600 °C for the localized fire stage.
- (b) The minimum value for the burner monitor during the engulfing fire stage ( $T_{min_{ENG25}}$ ) shall be calculated by subtracting 50 °C from the 60-second rolling average of  $T_{B_{ENG25}}$ . If the resultant minimum values exceed 800 °C, the minimum value is set to 800 °C for the engulfing fire stage.

If the above requirements are satisfactorily met, then the burner setup is typically ready for CHSS fire test.

5.4.5.5. If results are not satisfactory, then the source of the variation in burner performance shall be identified and corrected and then re-tested until the requirements for pre-test verification are met. Adjustment of the height is permissible to achieve acceptable operation within the allowable operating ranges as defined in Tables 7 and 8.

When the width/diameter of the CHSS test article is larger than the width of the burner and the shape of the bottom of the CHSS test article impedes the burner exhaust from readily flowing up and around the CHSS test article during the CHSS fire test, then the burner air flow can be restricted and the burner monitors may not be able to achieve the required minimum temperatures during the localized and/or engulfing fire stages of the CHSS fire test. If the CHSS test article is expected to impede the burner flow (or if the burner monitors did not achieve the required temperatures during the CHSS fire test), then the following additional pre-test is required to determine the appropriate height for mounting the CHSS test article above the burner such that required temperatures are achieved:

- (a) A pre-test plate (made of steel) with approximately the length and width/diameter of the CHSS test article is mounted above the burner to simulate the bottom on the CHSS test article at an initial height of 100 mm.
- (b) Burner monitors as defined in Annex 3, paragraph 5.4.3.2. are located  $25 \pm 5$  mm below the surface.

- (c) The burners are operated in the localized and engulfing modes (at the HRR/As established above) and the temperatures of the burner monitors are measured.
- (d) If the burner monitors for both the localized and engulfing fire stages do not meet the minimum criteria (defined in Annex 3, paragraph 5.4.5.4.), then the height of the pre-test plate above the burner shall be increased by 50 mm and the process in steps b and c are repeated until a satisfactory height is achieved.

NOTE: Satisfactory results are expected at heights of 200 – 250 mm.

If the burner monitors meet the minimum criteria (defined above) for both the localized and engulfing fire stages, then the required height for locating the CHSS test article above the burner has been determined and the pre-test is complete.

5.5. Mounting of the CHSS test article above the burner

After the pre-test checkout(s) have been satisfactorily completed, the CHSS test article shall be mounted above the burner.

5.5.1. Height and location of the CHSS test article above the burner

The CHSS test article shall be mounted at the same height above the burner as for the pre-test checkout in Annex 3, paragraph 5.4. and located over the burner such that nozzles on the two centrally-located manifolds (or "rails") are pointing toward the targeted region on the bottom (i.e., the lowest elevation) of the CHSS test article. See Figures 8 and 9 for examples of the mounting of cylindrical and conformable containers, respectively.

Figure 8  
Position the bottom of the cylindrical container relative to the burner

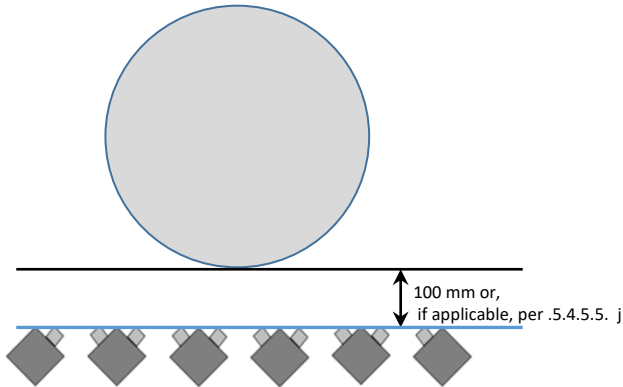
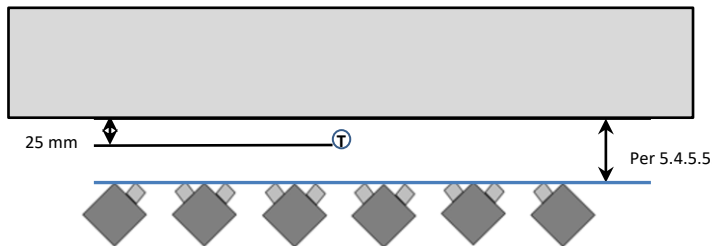


Figure 9  
Position the bottom of the conformable container relative to the burner



5.5.2. Targeting of the localized and engulfing burner zones on the CHSS



Localized fire shall be targeted on the CHSS test article to challenge the ability of the TPRDs to sense the fire and respond in order to protect the container. This requirement is met as follows:

- (a) For CHSS where the manufacturer has not opted to include vehicle-specific features (as defined in paragraph 5.1.), the CHSS test article shall be rotated relative to the localized burner to minimize the ability to TPRDs to sense the fire and respond. Shields, panels, wraps, structural elements, and other features added to the container shall be considered when establishing the worst case orientation relative to the localized fire as parts and features intended to protect sections of the container but can (inadvertently) leave other portions or joints/seams vulnerable to attack and/or hinder the ability of TPRDs to respond.

For CHSS where the manufacturer has opted to include vehicle-specific features (as defined in Annex 3, paragraph 5.1.), the CHSS test article is oriented relative to the localized burner to provide the worst case fire exposure identified for the specific vehicle.

- (b) The localized burner shall be located under the CHSS test article such that the distance from localized fire zone to the nearest TPRD sense point(s) is maximized.

The engulfing fire zone shall extend in one direction from the localized fire zone toward the nearest TPRD (or sense point). The engulfing burner can extend beyond the TPRD(s) if the distance from the localized burner is less than the maximum allowable extension of the engulfing burner as defined above (i.e.,  $1,400 \pm 50$  mm).

#### 5.6. Instrumentation and connections to the CHSS test article

- 5.6.1. The definition and mounting of the thermocouples for burner monitoring are analogous to Annex 3, paragraph 5.4.3.2. for the pre-test checkout. See Figures 8 and 9 for examples of the mounting below cylindrical and conformable containers, respectively.

At least one thermocouple for burner monitoring shall be located in the localized fire exposure of the CHSS test article, and two thermocouples shall be located in the extension of the engulfing fire exposure on the CHSS test article. Additional thermocouples may be added to back up or supplement burner monitoring along the centre line of the localized and engulfing burners.

- 5.6.2. The calculation of the burner monitor temperatures ( $T_{B_{LOC25}}$  and  $T_{B_{ENG25}}$ ) are analogous to the process in Annex 3, paragraph 5.4.3.3. for the pre-test checkout.

Additional thermocouples may be located at TPRD sensing points or any other locations for optional diagnostic purposes.

A fluid line shall be connected to the CHSS prior to test to allow fill and vent of the CHSS as defined within the test procedure.

Shut-off(s) valves shall be installed on the line as required to isolate the CHSS contents during the test and perform required fill and vent procedures prior to or after the test.

A pressure transmitter shall also be installed on the line such that the pressure of contents within the CHSS can be remotely monitored during the test. The accuracy of the transmitter shall be at least  $\pm 1$  per cent of full scale and  $\pm 10$  per cent at 1 MPa.

#### 5.7. The CHSS fire test procedure

- 5.7.1. Prior to conducting the CHSS fire test, the CHSS shall be filled with compressed hydrogen gas to  $\geq 100$  per cent of state-of-charge (SOC).

5.7.2. The first stage of the CHSS fire test is initiated by starting the fuel flow to the localized burner and igniting the burner:

- (a) After ignition is confirmed, the fuel flow is set to the value that matches the desired specific heat release rate (HRR/A) for the localized burner in Annex 3, paragraph 5.4.5.3., and the test time is set to 0 minutes.
- (b) As shown in Figure 4 in Annex 3, paragraph 5., the 10-second rolling average of the burner monitor in the localized fire zone ( $T_{B_{LOC25}}$ ) shall be at least 300 °C within 1 minute of ignition and for the next 2 minutes.

Within 3 minutes of start, the 60-second rolling average of the localized burner monitor ( $T_{B_{LOC25}}$ ) shall be greater than  $T_{min_{LOC25}}$  as determined in Annex 3, paragraph 5.4.5.4. If  $T_{B_{LOC25}}$  does not achieve the required temperature within 3 minutes, the test is terminated.

NOTES:

- (i) Monitoring of the 60-second rolling average of the localized burner monitor ( $T_{B_{LOC25}}$ ) is not required after the above criteria are met as the burner monitor readings may be compromised by expansion or falling of materials from the CHSS test article during subsequent CHSS fire test.
- (ii) The temperature outside the region of the localized fire exposure is not specified during these initial 10 minutes from the time of ignition.
- (iii) If the test is terminated because  $T_{B_{LOC25}}$  did not achieve required temperature within the required time, requirements in Annex 3, paragraph 5.2. for providing wind shielding and paragraph 5.4.5. for adjusting the burner operation and setup should be considered prior to re-test.

5.7.3. After 10 minutes from start of test, the second stage is initiated by starting fuel flow to the engulfing burner extension and igniting the burner:

- (a) After ignition is confirmed, the fuel flow rates to both the localized and engulfing fire extension are set to the value that matches the desired specific heat release (HRR/A) for the engulfing burner stage in Annex 3, paragraph 5.4.5.3.
- (b) Within 2 minutes of the start of ignition of the engulfing burner (i.e., within 12 minutes from start of test), the 60-second rolling average of the engulfing burner monitor ( $T_{B_{ENG25}}$ ) shall be equal or greater than  $T_{min_{ENG25}}$  as determined in Annex 3, paragraph 5.4.5.4.

NOTES:

- (i) Monitoring of the 60-second rolling average of the engulfing burner monitor ( $T_{B_{ENG25}}$ ) is not required after the above criteria are met as the burner monitor readings may be compromised by expansion or falling of materials from the CHSS test article during subsequent CHSS fire test.
- (ii) If the test is terminated because  $T_{B_{ENG25}}$  did not achieve required temperature within the required time, requirements in Annex 3, paragraph 5.2. for providing wind shielding and Annex 3, paragraph 5.4.5. for adjusting the burner operation and setup should be considered prior to re-test.

5.7.4. Minor movement of the CHSS test article and subsequent repositioning of the CHSS test article relative to the burners is allowed when TPRD(s) activate.

The fire test continues until either;

- (a) the CHSS vents and the pressure falls to less than 1 MPa; or

- (b) a total test of 1 hour from start of test is reached for CHSS in vehicles of categories M<sub>1</sub> and N<sub>1</sub> or 2 hours for CHSS in vehicles of categories M<sub>2</sub>, M<sub>3</sub>, N<sub>2</sub> and N<sub>3</sub>.

When the test is completed, the burner fuel flow shall be shut off within 1 minute, and the CHSS shall be depressurized (if not already near ambient pressure) and then purged with inert gas for safe post-test handling."

*Annex 4 (all paragraphs and Appendix).*, amend to read:

## "Annex 4

### Test procedures for specific components for the compressed hydrogen storage system

Testing is performed with either hydrogen or non-reactive gas as specified in the following paragraphs:

Hydrogen gas shall be compliant with ISO 14687:2019, SAE J2719\_202003, or meet the following specifications:

- (a) Hydrogen fuel index:  $\geq 99.97\%$
- (b) Total non-hydrogen gases:  $\leq 300 \mu\text{mol/mol}$
- (c) Water:  $\leq 5 \mu\text{mol/mol}$
- (d) Particle concentrations:  $\leq 1 \text{ mg/kg}$

The leak test gas shall be hydrogen, helium, or a non-reactive gas mixture containing a detectable amount of helium or hydrogen gas.

All tests are performed at ambient temperature of  $20 \pm 5 \text{ }^\circ\text{C}$  unless otherwise specified.

#### 1. TPRD Qualification Performance Tests

The TPRD qualification performance tests are specified as follows (see also Appendix 1):

##### 1.1. Pressure cycling test.

Five TPRD units undergo 15,000 internal pressure cycles according to Table 1. Following this test, the pressure relief device shall comply with the requirements of the leak test (Annex 4, paragraph 1.8.), the bench top activation test (Annex 4, paragraph 1.9.) and flow rate test (Annex 4, paragraph 1.10.). See Table 1 below for a summary of the pressure cycles.

Table 1  
**Pressure cycling conditions**

<i>Pressure cycles to per cent NWP</i>	<i>No. of cycles</i>	<i>Sample temperature for cycling</i>
$\leq 2 \text{ MPa to } \geq 150 \text{ per cent NWP}$	First 10	$\geq 85 \text{ }^\circ\text{C}$
$\leq 2 \text{ MPa to } \geq 125 \text{ per cent NWP}$	Next 2, 240	$\geq 85 \text{ }^\circ\text{C}$
$\leq 2 \text{ MPa to } \geq 125 \text{ per cent NWP}$	Next 10,000	$20 \text{ }^\circ\text{C}$
$\leq 2 \text{ MPa to } \geq 80 \text{ per cent NWP}$	Next 2,750	$\leq -40 \text{ }^\circ\text{C}$

Note: All cycles are conducted at a rate of  $\leq 10$  cycles per minute.

1.2. Accelerated life test.

Eight TPRD units undergo testing; three at the manufacturer's specified activation temperature,  $T_f$ , and five at an accelerated life temperature. The Accelerated Life test temperature is  $T_L$ , given in °C by the expression:

$$T_L = \left( \frac{0.502}{\beta + T_f} + \frac{0.498}{\beta + T_{ME}} \right)^{-1} - \beta$$

Where  $\beta = 273.15$ ,  $T_{ME}$  is 85 °C, and  $T_f$  is the manufacturer's specified activation temperature.

The TPRD is placed in an oven or liquid bath with the temperature held constant ( $\pm 1$  °C). The pressure on the TPRD inlet is  $\geq 125$  per cent NWP. The pressure supply may be located outside the controlled temperature oven or bath. Each device is pressurized individually or through a manifold system. If a manifold system is used, each pressure connection may include a check valve to prevent pressure depletion of the system when one specimen fails. The three TPRDs tested at  $T_f$  shall activate in less than 10 hours. The five TPRDs tested at  $T_L$  shall not activate in less than 500 hours and shall meet the requirements of Annex 4, paragraph 1.8. (Leak test).

1.3. Temperature cycling test

- (a) An unpressurized TPRD is placed in a liquid bath maintained at  $\leq -40$  °C for at least two hours. The TPRD is transferred to a liquid bath maintained at  $\geq +85$  °C within five minutes, and maintained at that temperature at least two hours. The TPRD is transferred to a liquid bath maintained at  $\leq -40$  °C within five minutes;
- (b) Step (a) is repeated until 15 thermal cycles have been achieved;
- (c) With the TPRD conditioned for at least two hours in the  $\leq -40$  °C liquid bath, the internal pressure of the TPRD is cycled with hydrogen or inert gas between  $\leq 2$  MPa and  $\geq 80$  per cent NWP for 100 cycles while the liquid bath is maintained at  $\leq -40$  °C;
- (d) Following the thermal and pressure cycling, the pressure relief device shall comply with the requirements of Leak test (Annex 4, paragraph 1.8.), except that the Leak test shall be conducted at  $\leq -40$  °C. After the leak test, the TPRD shall comply with the requirements of the bench top activation test (Annex 4, paragraph 1.9.) and then the flow rate test (Annex 4, paragraph 1.10.).

1.4. Salt corrosion resistance test

Accelerated cyclic corrosion shall be performed in accordance with the following procedure:

- (a) Three TPRDs shall be exposed to an accelerated laboratory corrosion test, under a combination of cyclic conditions (salt solution, various temperatures, humidity, and ambient environment). The test method is comprised of 1 per cent (approximate) complex salt mist applications coupled with high temperature, high humidity and high temperature dry off. One test cycle is equal to 24 hours, as illustrated in Table 2.

Table 2  
Accelerated Cyclic Corrosion Conditions (1 cycle = 24 h)

Cycle Condition	Temperature (°C)	Relative Humidity ( per cent)	Cycle Duration
Ambient stage	25 ± 3	45 ± 10	8 h ± 10 min
Transition 1 h ± 5 min			
Humid stage	49 ± 2	100	7 h ± 10 min

<i>Cycle Condition</i>	<i>Temperature (°C)</i>	<i>Relative Humidity ( per cent)</i>	<i>Cycle Duration</i>
Transition 3 h ± 10 min			
Dry stage	60 ± 2	≤ 30	5 h ± 10 min

- (b) The apparatus used for this test shall consist of a fog/environmental chamber, suitable water supply conforming to ASTM D1193-06(2018) Type IV, provisions for heating the chamber, and the necessary means of controlling temperature between 22 °C and 62 °C. The apparatus shall include provisions for a supply of suitably conditioned compressed air and one or more nozzles for fog generation. The nozzle or nozzles used for the generation of the fog shall be directed or baffled to minimize any direct impingement on the test samples.
- (c) The apparatus shall consist of the chamber design as defined in ISO 6270-2:2017. During "wet-bottom" generated humidity cycles, the proper wetness shall be confirmed by visual inspection of visible water droplets on the samples.
- (d) Steam generated humidity may be used provided the source of water used in generating the steam is free of corrosion inhibitors. During steam generated humidity cycles, the testing agency must confirm that visible water droplets are found on the samples to verify proper wetness.
- (e) The apparatus for the dry off stage shall have the ability to obtain and maintain the following environmental conditions: temperature: 60 ± 2 °C and humidity: ≤ 30 per cent RH. The apparatus shall also have sufficient air circulation to prevent temperature stratification, and also allow thorough drying of the test samples.
- (f) The force/impingement from this salt application shall not remove corrosion or damage the coatings/paints system of test samples.
- (g) The complex salt solution in percent by mass shall be as specified below:
- (i) Sodium Chloride (NaCl): 0.9 per cent
  - (ii) Calcium Chloride (CaCl<sub>2</sub>): 0.1 per cent
  - (iii) Sodium Bicarbonate (NaHCO<sub>3</sub>): 0.075 per cent

Sodium Chloride must be reagent grade or food grade. Calcium Chloride must be reagent grade. Sodium Bicarbonate must be reagent grade or food grade (e.g., Baking Soda or comparable product is acceptable). Water must meet ASTM D1193-06(2018) Type IV requirements.

NOTE: Either CaCl<sub>2</sub> or NaHCO<sub>3</sub> material must be dissolved separately in water and added to the solution of the other materials. If all solid materials are added dry, an insoluble precipitate may result.

- (h) The TPRD shall be installed in accordance with the manufacturer's recommended procedure and exposed to the cyclic corrosion test method described in Table 2.
- (i) Repeat the cycle daily until 100 cycles of exposure have been completed. For each salt mist application, the solution shall be sprayed as an atomized mist, using the spray apparatus to mist the components until all areas are thoroughly wet / dripping. Suitable application techniques include using a plastic bottle, or a siphon spray powered by oil-free regulated air to spray the test samples. The quantity of spray applied shall be sufficient to visibly rinse away salt accumulation left

from previous sprays. A total of four salt mist applications shall be applied during the ambient stage. Salt mist is not applied during any other stage of the test. The first salt mist application occurs at the beginning of the ambient stage. Each subsequent salt mist application shall be applied approximately ninety minutes after the previous application in order to allow adequate time for test sample to dry. If the test must be interrupted for weekends and holidays, the test article shall be kept at the ambient temperature of  $25 \pm 3$  °C and the relative humidity of  $45 \pm 10$  per cent and the cycle shall restart from ambient stage.

- (j) Humidity ramp times between the ambient and wet condition, and between the wet and dry conditions, can have a significant effect on test acceleration (this is because corrosion rates are highest during these transition periods). The time from ambient to the wet condition shall be  $60 \pm 5$  minutes and the transition time between wet and dry conditions shall be  $180 \pm 10$  minutes.
- (k) Immediately after the corrosion test, the samples are rinsed with fresh tap water and allowed to dry before evaluating.
- (l) The TPRDs shall then comply with the requirements of the leak test (Annex 4, paragraph 1.8.), bench top activation test (Annex 4, paragraph 1.9.) and flow rate test (Annex 4, paragraph 1.10.).

#### 1.5. Vehicle environment test

Resistance to degradation by external exposure to automotive fluids is determined by the following test:

- (a) The inlet and outlet connections of the TPRD are connected or capped in accordance with the manufacturers installation instructions. The external surfaces of the TPRD are exposed for 24 hours at ambient temperature to each of the following fluids:
  - (i) Sulphuric acid (19 per cent solution by volume in water);
  - (ii) Ethanol/gasoline – 10 per cent/90 per cent concentration of E10 fuel; and
  - (iii) Windshield washer fluid (50 per cent by volume methyl alcohol and water).

The fluids are replenished as needed to ensure complete exposure for the duration of the test. A distinct test is performed with each of the fluids. One TPRD shall be used for exposure to all of the fluids in sequence.

- (b) After exposure to each fluid, the TPRD is wiped off and rinsed with water;
- (c) The TPRD shall not show signs of physical degradation that could impair the function of the TPRD, specifically: cracking, softening, or swelling. Cosmetic changes such as pitting or staining are not failures. At the conclusion of all exposures, the TPRD shall comply with the requirements of the leak test (Annex 4, paragraph 1.8.), bench top activation test (Annex 4, paragraph 1.9.) and flow rate test (Annex 4, paragraph 1.10.).

#### 1.6. Stress corrosion cracking test.

This test is applicable to TPRDs containing copper alloys exposed to the outside environment.

For TPRDs containing components made of a copper alloy (e.g. brass), one TPRD unit is tested. All copper alloy components exposed to the atmosphere

shall be degreased and then continuously exposed for at least ten days to a moist ammonia-air mixture maintained in a glass chamber having a glass cover.

Aqueous ammonia having a specific gravity of 0.94 is maintained at the bottom of the glass chamber below the sample at a concentration of at least 20 ml per litre of chamber volume. The sample is positioned  $35 \pm 5$  mm above the aqueous ammonia solution and supported in an inert tray. The moist ammonia-air mixture is maintained at atmospheric pressure at  $35 \pm 5^\circ\text{C}$ . Copper alloy components shall not exhibit cracking or delaminating due to this test.

#### 1.7. Drop and vibration test

- (a) TPRD units representative of their final assembled form are dropped from a height of 2 m or greater without restricting its motion as a result of gravity, at ambient temperature onto a smooth concrete surface. The TPRD is allowed to bounce on the concrete surface after the initial impact.

Up to six separate units may be used such that all six of the major axes are covered (i.e. one direction drop per sample, covering the opposing directions of 3 orthogonal axes: vertical, lateral and longitudinal). At the manufacturer's discretion, one unit may be dropped in all six orientations.

After each drop, the sample shall be examined for visible damage. Any of the six dropped orientations that do not have exterior damage that indicates that the part is unsuitable for use (i.e. threads damaged sufficiently that part is rendered unusable), shall proceed to step (b).

Note: any samples with damage from the drop that results in the TPRD not being able to be installed (i.e. thread damage) shall not proceed to step (b) and shall not be considered a failure of this test;

- (b) Each of the TPRD units dropped in step (a) that did not have visible damage and one additional unit not subjected to a drop are mounted in a test fixture in accordance with manufacturer's installation instructions and vibrated 30 minutes along each of the three orthogonal axes (vertical, lateral and longitudinal) at the most severe resonant frequency for each axis. The most severe resonant frequencies are determined using an acceleration of 1.5 g and sweeping through a sinusoidal frequency range of 10 to 500 Hz in 10 minutes. The resonance frequency is identified by a pronounced increase in vibration amplitude. If the resonance frequency is not found in this range, the test shall be conducted at 40 Hz. Following this test, each sample shall subsequently comply with the requirements of the leak test (Annex 4, paragraph 1.8.), bench top activation test (Annex 4, paragraph 1.9.) and flow rate test (Annex 4, paragraph 1.10.).

#### 1.8. Leak test

This test applies to one TPRD that has not undergone previous design qualification tests and additional units as specified in other tests in Annex 4, paragraph 1. The leak test is performed at ambient, high and low temperatures. The unit shall be thermally conditioned at each of the required test temperatures and held pressurized to  $\geq 2$  MPa for at least one hour to ensure thermal stability before testing. The TRPD is pressurized with leak test gas at the inlet. The test conditions are:

- (a) Ambient temperature: condition the unit at ambient temperature; test at  $2 \pm 0.5$  MPa and  $\geq 125$  per cent NWP;
- (b) High temperature: condition the unit at  $\geq 85^\circ\text{C}$ ; test at  $2 \pm 0.5$  MPa and  $\geq 125$  per cent NWP;

- (c) Low temperature: condition the unit at  $\leq -40$  °C; test at  $2 \pm 0.5$  MPa and  $\geq 100$  per cent NWP.

Following conditioning at each of the specified test temperatures, the unit is observed for leakage while immersed in a temperature-controlled fluid (or equivalent method) for at least one minute at each of the test pressures listed above. If no bubbles are observed for the specified time period, the sample passes the test. If bubbles are detected, the leak rate is measured. The total hydrogen leak rate shall be less than 10 Nml/h.

1.9. Bench top activation test

Three new TPRD units are tested without being subjected to other design qualification tests in order to establish a baseline time for activation, which is defined as the averaged activation time of these three units. Additional pre-tested units (pre-tested according to Annex 4, paragraphs 1.1., 1.3., 1.4., 1.5. and 1.7.) undergo bench top activation testing as specified in other tests in Annex 4, paragraph 1.

- (a) The test setup consists of either an oven or chimney which is capable of controlling air temperature and flow to achieve  $600 \pm 10$ °C in the air surrounding the TPRD. The TPRD unit is not exposed directly to flame. The TPRD unit is mounted in a fixture according to the manufacturer's installation instructions; the test configuration is to be documented;
- (b) A thermocouple is placed in the oven or chimney to monitor the temperature. The temperature shall remain within the acceptable range for at least two minutes prior to running the test;
- (c) Prior to insertion, the TPRD unit is pressurized to  $2 \pm 0.5$  MPa;
- (d) The pressurized TPRD unit is inserted into the oven or chimney, and the time for the device to activate is recorded;
- (e) TPRD units previously subjected to other tests in Annex 4, paragraph 1. shall activate within a period no more than two minutes longer than the baseline activation time;
- (f) The maximum difference in the activation time of the three TPRD units that had not undergone previous testing shall be no more than two minutes.

1.10. Flow rate test

- (a) Eight TPRD units are tested for flow capacity. The eight units consist of three new TPRD units and one TPRD unit from each of the following previous tests: Annex 4, paragraphs 1.1., 1.3., 1.4., 1.5. and 1.7.;
- (b) Each TPRD unit is activated according to Annex 4, paragraph 1.9. After activation and without cleaning, removal of parts, or reconditioning, each TPRD unit is subjected to a flow test;
- (c) Flow rate testing is conducted with an inlet pressure of  $2 \pm 0.5$  MPa. The outlet is at ambient pressure. The inlet pressure and flow rate are recorded;
- (d) Flow rate is measured with accuracy within  $\pm 2$  per cent. The lowest measured value of the eight pressure relief devices shall not be less than 90 per cent of the highest flow value.

1.11. Atmospheric exposure test

The atmospheric exposure test applies to qualification of TPRDs if the component has non-metallic materials exposed to the atmosphere during normal operating conditions.

- (a) All non-metallic materials that provide a fuel containing seal, and that are exposed to the atmosphere, for which a satisfactory declaration of



properties is not submitted by the applicant, shall not crack or show visible evidence of deterioration after exposure to oxygen for at least 96 hours at 70 °C and 2 MPa in accordance with ISO 188:2011 or ASTM D572-04(2019);

- (b) All elastomers that are exposed to the atmosphere shall demonstrate resistance to ozone by one or more of the following:
  - (i) Specification of elastomer compounds with established resistance to ozone;
  - (ii) Component testing in accordance with ISO 1431-1:2012, ASTM D1149-18, or equivalent test methods;
  - (iii) The test piece shall be stressed to 20 per cent elongation, exposed to air at 40 °C with an ozone concentration of 50 parts per hundred million for 120 hours. The non-metallic materials in the test piece shall not crack or show visible evidence of deterioration after exposure to ozone.

## 2. Tests for check valve and shut-off valve

The check valve and shut-off valve qualification performance tests are specified as follows (see also Appendix 2):

### 2.1. Hydrostatic strength test

The outlet opening in components is plugged and valve seats or internal blocks are made to assume the open position. One unit is tested without being subjected to other design qualification tests in order to establish a baseline burst pressure. Other units are tested as specified in subsequent tests of Annex 4, paragraph 2.

- (a) A hydrostatic pressure of  $\geq 250$  per cent NWP is applied to the inlet of the component for at least three minutes. The component is examined to ensure that rupture has not occurred;
- (b) The hydrostatic pressure is then increased at a rate of  $\leq 1.4$  MPa/s until component failure. The hydrostatic pressure at failure is recorded. The failure pressure of previously tested units shall be  $\geq 80$  per cent of the failure pressure of the baseline, unless the hydrostatic pressure exceeds 400 per cent NWP.

### 2.2. Leak test

This test applies to one unit that has not undergone previous design qualification tests and additional units as specified in other tests in Annex 4, paragraph 2. The leak test is performed at ambient, high and low temperatures. The unit shall be thermally conditioned at each of the required test temperatures and held pressurized to  $\geq 2$  MPa for at least one hour to ensure thermal stability before testing. The outlet opening is plugged with the appropriate mating connection and pressurized leak test gas is applied to the inlet. The required test conditions are:

- (a) Ambient temperature: condition the unit at  $20 \pm 5$  °C; test at  $2 \pm 0.5$  MPa and  $\geq 125$  per cent NWP;
- (b) High temperature: condition the unit at  $\geq 85$  °C; test at  $2 \pm 0.5$  MPa and  $\geq 125$  per cent NWP;
- (c) Low temperature: condition the unit at  $\leq -40$  °C; test at  $2 \pm 0.5$  MPa and  $\geq 100$  per cent NWP.

Following conditioning at each of the specified test temperatures, the unit is observed for leakage while immersed in a temperature-controlled fluid (or equivalent method) for at least one minute at each of the test pressures listed above. If no bubbles are observed for the specified time period, the sample

passes the test. If bubbles are detected, the leak rate is measured by an appropriate method. The leak rate shall not exceed 10 Nml/h of hydrogen gas.

### 2.3. Extreme temperature pressure cycling test

The total number of operational cycles is 15,000 for the check valve and 50,000 for the shut-off valve. The valve unit is installed in a test fixture corresponding to the manufacturer's specifications for installation.

- (a) The operation of the unit is continuously repeated using hydrogen or non-reactive gas at all specified temperatures and pressures as follows:
  - (i) Ambient temperature cycling. The unit undergoes 90 per cent of the total operational cycles at  $\geq 100$  per cent NWP with the part stabilized at ambient temperature;
  - (ii) High temperature cycling. The unit then undergoes 5 per cent of the total operational cycles at  $\geq 125$  per cent NWP with the part stabilized at  $\geq 85^{\circ}\text{C}$ ;
  - (iii) Low temperature cycling. The unit then undergoes 5 per cent of the total operational cycles at  $\geq 80$  per cent NWP with the part stabilized at  $\leq -40^{\circ}\text{C}$ .
- (b) The operational cycle requirements shall be as follows:
  - (i) Check valve: A check valve shall be capable of withstanding 15,000 cycles of operation, and at least 24 hours of chatter flow when submitted to the following test procedure. The check valve shall be connected to a test fixture. The required test pressure is applied in six pulses to the inlet of the check valve with the outlet closed. The pressure shall then be vented from the check valve inlet. Failure of the check valve to reseal and prevent backflow shall constitute failure of the check valve. The pressure shall then be lowered on the check valve outlet side to  $\leq 60$  per cent of NWP prior to the next cycle. Following the operation cycles, the check valve shall be subjected to at least 24 hours of chatter flow at a flow rate that causes the most chatter (valve flutter). At the completion of the test, the check valve shall comply with the leak test (Annex 4, paragraph 2.2.) and hydrostatic strength test (Annex 4, paragraph 2.1.);
  - (ii) Shut-off valve: A shut-off valve shall be capable of withstanding 50,000 cycles of operation when submitted to the following test procedure. The shut-off valve shall be mounted into a suitable test fixture. Each cycle shall consist of filling through the inlet port to the required test pressure. The shut-off valve shall then be opened (energized) and the pressure in the valve/fixture reduced to 50 percent of the filling test pressure. The shut-off valve shall then be closed (de-energized) prior to the next filling cycle.

Following the operation cycles, the shut-off valve shall be subjected to at least 24 hours of chatter flow at a flow rate that is within normal operating conditions that causes chatter (valve flutter), only if the shut-off valve is functioning as a check valve during fuelling.

Note: If no chatter is induced during normal flow rates, this 24 h chatter flow test is not required.

At the completion of the test the shut-off valve shall comply with the leak test Annex 4, paragraph 2.2.) and hydrostatic strength test Annex 4, paragraph 2.1.).

### 2.4. Salt corrosion resistance test

Accelerated cyclic corrosion shall be performed in accordance with the following procedure:

- (a) Three component samples shall be exposed to an accelerated laboratory corrosion test, under a combination of cyclic conditions (salt solution, various temperatures, humidity, and ambient environment). The test method is comprised of 1 per cent (approximate) complex salt mist applications coupled with high temperature, high humidity and high temperature dry off. One test cycle is equal to 24 hours, as illustrated in Table 3.

Table 3  
**Accelerated Cyclic Corrosion Conditions (1 cycle = 24 h)**

<i>Cycle Condition</i>	<i>Temperature (°C)</i>	<i>Relative Humidity ( per cent)</i>	<i>Cycle Duration)</i>
Ambient stage Transition 1 h ± 5 min	25 ± 3	45 ± 10	8 h ± 10 min
Humid stage Transition 3 h ± 10 min	49 ± 2	100	7 h ± 10 min
Dry stage	60 ± 2	≤ 30	5 h ± 10 min

- (b) The apparatus used for this test shall consist of a fog/environmental chamber, suitable water supply conforming to ASTM D1193-06(2018) Type IV, provisions for heating the chamber, and the necessary means of controlling temperature between 22 °C and 62 °C. The apparatus shall include provisions for a supply of suitably conditioned compressed air and one or more nozzles for fog generation. The nozzle or nozzles used for the generation of the fog shall be directed or baffled to minimize any direct impingement on the test samples.
- (c) The apparatus shall consist of the chamber design as defined in ISO 6270-2:2017. During "wet-bottom" generated humidity cycles, the testing agency must confirm that visible water droplets are found on the samples to verify proper wetness.
- (d) Steam generated humidity may be used provided the source of water used in generating the steam is free of corrosion inhibitors. During steam generated humidity cycles, the proper wetness shall be confirmed by visual inspection of visible water droplets on the samples.
- (e) The apparatus for the dry off stage shall have the ability to obtain and maintain the following environmental conditions: temperature: 60 ± 2 °C and humidity: ≤ 30 percent RH. The apparatus shall also have sufficient air circulation to prevent temperature stratification, and also allow thorough drying of the test samples.
- (f) The force/impingement from this salt application shall not remove corrosion or damage the coatings/paints system of test samples.
- (g) The complex salt solution in percent by mass shall be as specified below:
- (i) Sodium Chloride (NaCl): 0.9 per cent;
  - (ii) Calcium Chloride (CaCl<sub>2</sub>): 0.1 per cent;
  - (iii) Sodium Bicarbonate (NaHCO<sub>3</sub>): 0.075 per cent;

Sodium Chloride must be reagent grade or food grade. Calcium Chloride must be reagent grade. Sodium Bicarbonate must be reagent or food grade (e.g., Baking Soda or comparable product is acceptable). Water must meet ASTM D1193-06(2018) Type IV requirements.

NOTE: Either  $\text{CaCl}_2$  or  $\text{NaHCO}_3$  material must be dissolved separately in water and added to the solution of the other materials. If all solid materials are added dry, an insoluble precipitate may result.

- (h) The component samples shall be installed in accordance with the manufacturer's recommended procedure and exposed to the cyclic corrosion test method described in Table 3.
- (i) Repeat the cycle daily until 100 cycles of exposure have been completed. For each salt mist application, the solution shall be sprayed as an atomized mist, using the spray apparatus to mist the components until all areas are thoroughly wet / dripping. Suitable application techniques include using a plastic bottle, or a siphon spray powered by oil-free regulated air to spray the test samples. The quantity of spray applied shall be sufficient to visibly rinse away salt accumulation left from previous sprays. A total of four salt mist applications shall be applied during the ambient stage. Salt mist is not applied during any other stage of the test. The first salt mist application occurs at the beginning of the ambient stage. Each subsequent salt mist application shall be applied approximately ninety minutes after the previous application in order to allow adequate time for test sample to dry. If the test must be interrupted for weekends and holidays, the test article shall be kept at the ambient temperature of  $25 \pm 3$  °C and the relative humidity of  $45 \pm 10$  per cent and the cycle shall restart from ambient stage.
- (j) Humidity ramp times between the ambient and wet condition, and between the wet and dry conditions, can have a significant effect on test acceleration (this is because corrosion rates are highest during these transition periods). The time from ambient to the wet condition shall be  $60 \pm 5$  minutes and the transition time between wet and dry conditions shall be  $180 \pm 5$  minutes.
- (k) Immediately after the corrosion test, the sample is rinsed with fresh tap water and allowed to dry before evaluating.
- (l) The tested samples shall then be subjected to the leak test (Annex 4, paragraph 2.2.) and hydrostatic strength test (Annex 4, paragraph 2.1.)

## 2.5. Vehicle environment test

Resistance to degradation by exposure to automotive fluids is determined by the following test.

- (a) The inlet and outlet connections of the valve unit are connected or capped in accordance with the manufacturers installation instructions. The external surfaces of the valve unit are exposed for at least 24 hours at ambient temperature to each of the following fluids:
  - (i) Sulphuric acid -19 per cent solution by volume in water;
  - (ii) Ethanol/gasoline – 10 per cent/90 per cent concentration of E10 fuel; and
  - (iii) Windshield washer fluid (50 per cent by volume methyl alcohol and water).

The fluids are replenished as needed to ensure complete exposure for the duration of the test. A distinct test is performed with each of the fluids. One component may be used for exposure to all of the fluids in sequence.

- (b) After exposure to each chemical, the component is wiped off and rinsed with water;

- (c) The component shall not show signs of physical degradation that could impair the function of the component, specifically: cracking, softening, or swelling. Cosmetic changes such as pitting or staining are not failures. At the conclusion of all exposures, the unit(s) shall comply with the requirements of the leak test (Annex 4, paragraph 2.2.) and hydrostatic strength test (Annex 4, paragraph 2.1.).

#### 2.6. Atmospheric exposure test

The atmospheric exposure test applies to qualification of check valve and shut-off valves if the component has non-metallic materials exposed to the atmosphere during normal operating conditions.

- (a) All non-metallic materials that provide a fuel containing seal, and that are exposed to the atmosphere, for which a satisfactory declaration of properties is not submitted by the applicant, shall not crack or show visible evidence of deterioration after exposure to oxygen for at least 96 hours at 70 °C and 2 MPa in accordance with ISO 188:2011 or ASTM D572-04 (2019);
- (b) All elastomers shall demonstrate resistance to ozone by one or more of the following:
  - (i) Specification of elastomer compounds with established resistance to ozone;
  - (ii) Component testing in accordance with ISO 1431-1:2012, ASTM D1149-1, or equivalent test methods;
  - (iii) The test piece, shall be stressed to 20 per cent elongation, exposed to air at 40 °C with an ozone concentration of 50 parts per hundred million during 120 h. The non-metallic materials in the test piece shall not crack or show visible evidence of deterioration after exposure to ozone.

#### 2.7. Electrical Tests

The electrical tests apply to qualification of the shut-off valve; they do not apply to qualification of check valves.

- (a) Abnormal voltage test. The solenoid valve is connected to a variable DC voltage source. The solenoid valve is operated as follows:
  - (i) An equilibrium (steady state temperature) hold is established for at least one hour at  $\geq 1.5$  times the rated voltage;
  - (ii) The voltage is increased to  $\geq 2$  times the rated voltage or 60 volts, whichever is less, and held for at least one minute;
  - (iii) Any failure shall not result in external valve leakage in accordance with Annex 4, paragraph 2.2., open valve or other unsafe conditions such as smoke, fire or melting.
- (b) Insulation resistance test. 1,000 V D.C. is applied between the power conductor and the component casing for at least two seconds. The minimum allowable resistance for that component is 240 k $\Omega$ .

#### 2.8. Vibration test

The valve unit is pressurized to  $\geq 100$  per cent NWP sealed at both ends, and vibrated for 30 minutes along each of the three orthogonal axes (vertical, lateral and longitudinal) at the most severe resonant frequencies. The most severe resonant frequencies are determined by acceleration of 1.5 g with a sweep time of at least 10 minutes within a sinusoidal frequency range of 10 to 500 Hz. If the resonance frequency is not found in this range the test is conducted at 40Hz. Following this test, each sample shall not show visible exterior damage that indicates that the performance of the part is compromised. At the completion

of the test, the unit shall comply with the requirements of the leak test specified in Annex 4, paragraph 2.2. and hydrostatic strength test specified in Annex 4, paragraph 2.1.

2.9. Stress corrosion cracking test

This test is applicable to valve units containing copper alloys exposed to the outside environment.

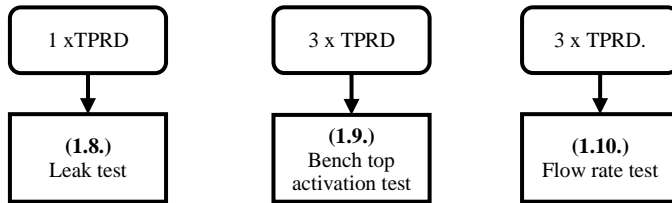
For the valve units containing components made of a copper alloy (e.g. brass), one valve unit is tested. The valve unit is disassembled, all copper alloy components are degreased and then the valve unit is reassembled before it is continuously exposed for at least 10 days to a moist ammonia-air mixture maintained in a glass chamber having a glass cover.

Aqueous ammonia having a specific gravity of 0.94 is maintained at the bottom of the glass chamber below the sample at a concentration of at least 20 ml per litre of chamber volume. The sample is positioned  $35 \pm 5$  mm above the aqueous ammonia solution and supported in an inert tray. The moist ammonia-air mixture is maintained at atmospheric pressure at  $35 \pm 5$  °C. Copper alloy components shall not exhibit cracking or delaminating due to this test.

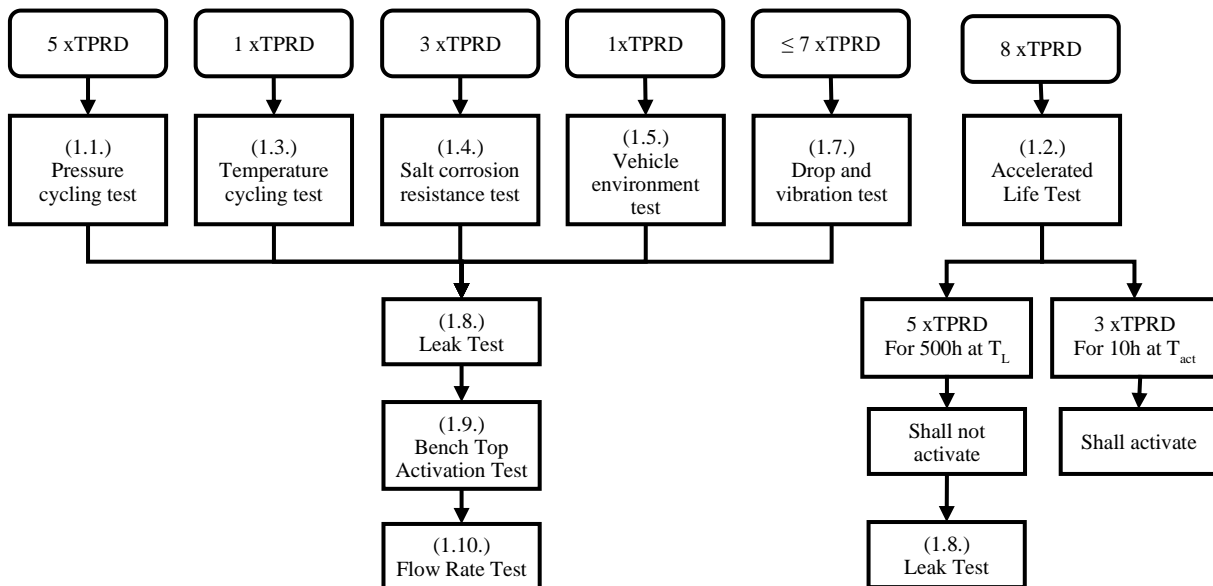
## Annex 4 - Appendix 1

### Overview of TPRD tests

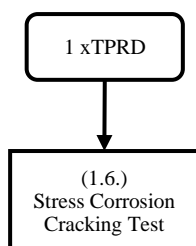
#### Baseline tests



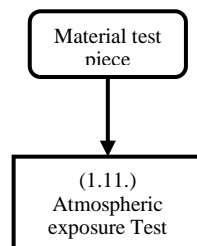
#### Performance and stress tests



Only for TPRD with copper based alloys:



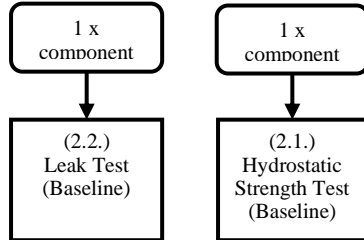
Only for TPRD with non-metallic materials:



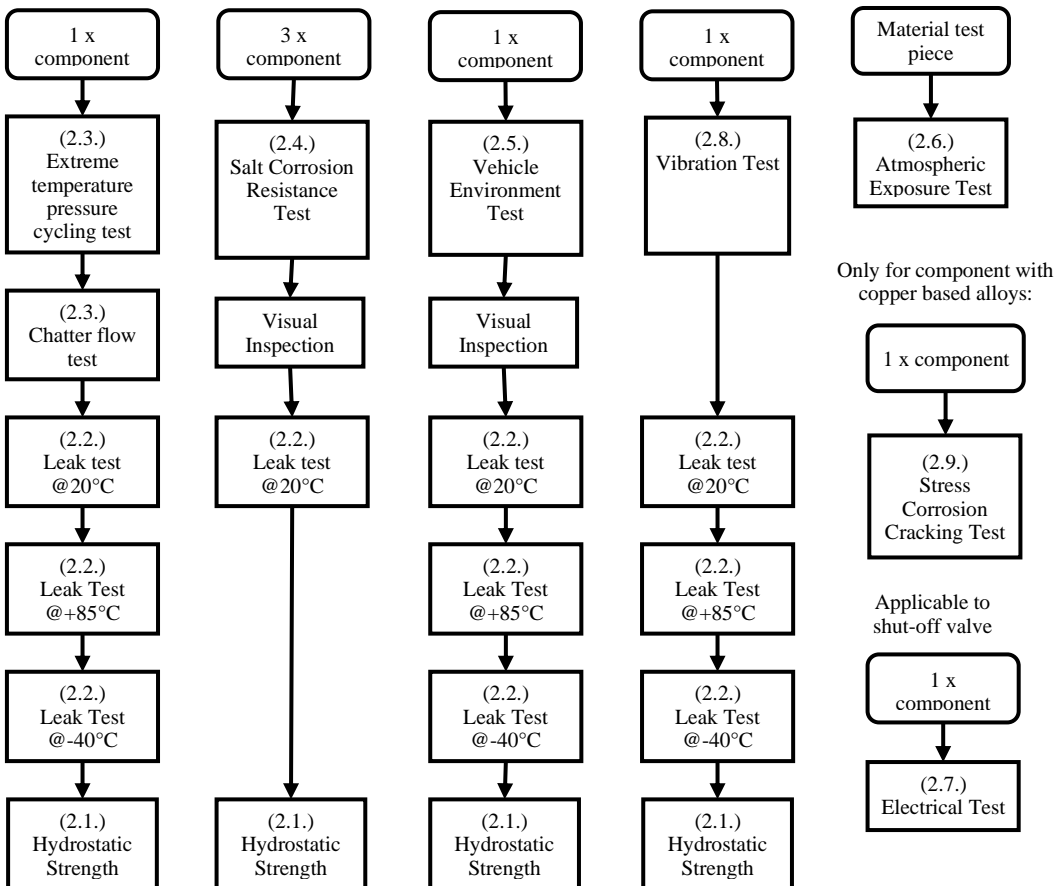
## Annex 4 - Appendix 2

### Overview of check valve and automatic shut-off valve tests

#### Baseline Tests



#### Performance and Stress Tests





Annex 5, paragraphs 1. to 3., amend to read:

"1. Post-crash compressed hydrogen storage system leak test

The crash tests used to evaluate post-crash hydrogen leakage are those set out in paragraph 7.2. of this Regulation.

Prior to conducting the crash test, instrumentation is installed in the CHSS to perform the required pressure and temperature measurements if the standard vehicle does not already have instrumentation with the required accuracy.

The CHSS is then purged, if necessary, following manufacturer's directions to remove impurities from the container before filling the CHSS with compressed hydrogen or helium gas. Since the storage system pressure varies with temperature, the targeted fill pressure is a function of the temperature. The target pressure shall be determined from the following equation:

$$P_{\text{target}} = \text{NWP} \times (273 + T_0) / 288$$

where NWP is the Nominal Working Pressure (MPa),  $T_0$  is the ambient temperature to which the storage system is expected to settle, and  $P_{\text{target}}$  is the targeted fill pressure after the temperature settles.

The container is filled to a minimum of 95 per cent of the targeted fill pressure and allowed to settle (stabilize) prior to conducting the crash test.

The main stop valve and shut-off valves for hydrogen gas, located in the downstream hydrogen gas piping, are in the normal driving condition kept open immediately prior to the impact.

1.1. Post-crash leak test: compressed hydrogen storage system filled with compressed hydrogen

The hydrogen gas pressure,  $P_0$  (MPa) and temperature,  $T_0$  (°C) are measured immediately before the impact and then at a time interval,  $\Delta t$  (min), after the impact. The time interval,  $\Delta t$ , starts when the vehicle comes to rest after the impact and continues for at least 60 minutes. The time interval,  $\Delta t$ , shall be increased, if necessary, to accommodate measurement accuracy for a storage system with a large volume operating up to 70MPa; in that case,  $\Delta t$  is calculated from the following equation:

$$\Delta t = V_{\text{CHSS}} \times \text{NWP} / 1,000 \times ((-0.027 \times \text{NWP} + 4) \times R_s - 0.21) - 1.7 \times R_s$$

where  $R_s = P_s / \text{NWP}$ ,  $P_s$  is the pressure range of the pressure sensor (MPa), NWP is the Nominal Working Pressure (MPa),  $V_{\text{CHSS}}$  is the volume of the CHSS (L), and  $\Delta t$  is the time interval (min). If the calculated value of  $\Delta t$  is less than 60 minutes,  $\Delta t$  is set to 60 minutes.

The initial mass of hydrogen in the CHSS is calculated as follows:

$$P_0' = P_0 \times 288 / (273 + T_0)$$

$$\rho_0' = -0.0027 \times (P_0')^2 + 0.75 \times P_0' + 1.07$$

$$M_0 = \rho_0' \times V_{\text{CHSS}}$$

The final mass of hydrogen in the CHSS,  $M_f$ , at the end of the time interval,  $\Delta t$ , is calculated as follows:

$$P_f' = P_f \times 288 / (273 + T_f)$$

$$\rho_f' = -0.0027 \times (P_f')^2 + 0.75 \times P_f' + 1.07$$

$$M_f = \rho_f' \times V_{\text{CHSS}}$$

where  $P_f$  is the measured final pressure (MPa) at the end of the time interval, and  $T_f$  is the measured final temperature (°C).

The average hydrogen flow rate over the time interval (that shall be less than the criteria in paragraph 7.2.1.) is therefore

$$V_{H_2} = (M_f - M_o) / \Delta t \times 22.41 / 2.016 \times (P_{\text{target}} / P_o)$$

where  $V_{H_2}$  is the average volumetric flow rate (NL/min) over the time interval and the term  $(P_{\text{target}} / P_o)$  is used to compensate for differences between the measured initial pressure,  $P_o$ , and the targeted fill pressure  $P_{\text{target}}$ .

- 1.2. Post-crash leak test: compressed hydrogen storage system filled with compressed helium

The helium gas pressure,  $P_0$  (MPa), and temperature  $T_0$  (°C), are measured immediately before the impact and then at a predetermined time interval after the impact. The time interval,  $\Delta t$ , starts when the vehicle comes to rest after the impact and continues for at least 60 minutes. The time interval,  $\Delta t$ , shall be increased if necessary in order to accommodate measurement accuracy for a CHSS with a large volume operating up to 70MPa; in that case,  $\Delta t$  is calculated from the following equation:

$$\Delta t = V_{\text{CHSS}} \times \text{NWP} / 1,000 \times ((-0.028 \times \text{NWP} + 5.5) \times R_s - 0.3) - 2.6 \times R_s$$

where  $R_s = P_s / \text{NWP}$ ,  $P_s$  is the pressure range of the pressure sensor (MPa),  $\text{NWP}$  is the Nominal Working Pressure (MPa),  $V_{\text{CHSS}}$  is the volume of the CHSS (L), and  $\Delta t$  is the time interval (min). If the value of  $\Delta t$  is less than 60 minutes,  $\Delta t$  is set to 60 minutes.

The initial mass of helium in the CHSS is calculated as follows:

$$P_o' = P_o \times 288 / (273 + T_o)$$

$$\rho_o' = -0.0043 \times (P_o')^2 + 1.53 \times P_o' + 1.49$$

$$M_o = \rho_o' \times V_{\text{CHSS}}$$

The final mass of helium in the CHSS,  $M_f$ , at the end of the time interval,  $\Delta t$ , is calculated as follows:

$$P_f' = P_f \times 288 / (273 + T_f)$$

$$\rho_f' = -0.0043 \times (P_f')^2 + 1.53 \times P_f' + 1.49$$

$$M_f = \rho_f' \times V_{\text{CHSS}}$$

where  $P_f$  is the measured final pressure (MPa) at the end of the time interval, and  $T_f$  is the measured final temperature (°C).

The average helium flow rate over the time interval is therefore

$$V_{\text{He}} = (M_f - M_o) / \Delta t \times 22.41 / 4.003 \times (P_{\text{target}} / P_o)$$

where  $V_{\text{He}}$  is the average volumetric flow rate (NL/min) over the time interval and the term  $P_{\text{target}} / P_o$  is used to compensate for differences between the measured initial pressure ( $P_o$ ) and the targeted fill pressure ( $P_{\text{target}}$ ).

Conversion of the average volumetric flow of helium to the average hydrogen flow is calculated with the following expression:

$$V_{H_2} = V_{\text{He}} / 0.75$$

where  $V_{H_2}$  is the corresponding average volumetric flow of hydrogen (that shall be less than the requirements in paragraph 7.2.1. of this Regulation to comply with).

2. Post-crash concentration test for enclosed spaces

The measurements are recorded in the crash test that evaluates potential hydrogen (or helium) leakage (Annex 5, paragraph 1. test procedure).

Sensors are selected to measure either the build-up of the hydrogen or helium gas or the reduction in oxygen (due to displacement of air by leaking hydrogen/helium).

Sensors are calibrated to traceable references to ensure an accuracy of  $\pm 5$  per cent at the targeted criteria of 4.0 per cent hydrogen or 3.0 per cent helium by volume in air, and a full-scale measurement capability of at least 25 per cent above the target criteria. The sensor shall be capable of a 90 per cent response to a full-scale change in concentration within 10 seconds.

Prior to the crash impact, the sensors are located in the passenger and luggage compartments of the vehicle as follows:

- (a) At a distance within 250 mm of the headliner above the driver's seat or near the top centre the passenger compartment;
- (b) At a distance within 250 mm of the floor in front of the rear (or rear most) seat in the passenger compartment;
- (c) At a distance within 100 mm of the top of luggage compartment within the vehicle that are not directly affected by the particular crash impact to be conducted.

The sensors are securely mounted on the vehicle structure or seats and protected for the planned crash test from debris, air bag exhaust gas and projectiles. The measurements following the crash are recorded by instruments located within the vehicle or by remote transmission.

The vehicle may be located either outdoors in an area protected from the wind and possible solar effects or indoors in a space that is large enough or ventilated to prevent the build-up of hydrogen to more than 10 per cent of the targeted criteria in the passenger and luggage compartments.

Post-crash data collection in enclosed spaces commences when the vehicle comes to a rest. Data from the sensors are collected at least every 5 seconds and continue for a period of 60 minutes after the test. A first-order lag (time constant) up to a maximum of 5 seconds may be applied to the measurements to provide "smoothing" and filter the effects of spurious data points.

The filtered readings from each sensor shall be below the targeted criteria of 4.0 per cent for hydrogen or 3.0 per cent for helium at all times throughout the 60 minutes post-crash test period.

### 3. Compliance test for single failure conditions

For requirement of paragraph 7.1.4.2., test procedure of Annex 5, paragraph 3.2. shall be executed.

For requirement of paragraph 7.1.4.3., test procedure of Annex 5, paragraph 3.1. or paragraph 3.2. shall be executed:"

*Annex 5, paragraph 3.1.1.2., amend to read:*

- "3.1.1.2. Test gas: Two mixtures of air and hydrogen gas: > 3.0 per cent concentration of hydrogen in the air to verify function of the warning, and > 4.0 per cent concentration of hydrogen in the air to verify the shut-down function. The proper concentrations are selected based on the recommendation (or the detector specification) by the manufacturer.

NOTE: The storage of pre-mixed gases of greater than 2 per cent hydrogen in air in compressed gas cylinders may be restricted or prohibited in various jurisdictions where test laboratories are located. As an alternative, gas mixtures up to 4 per cent hydrogen in-situ within the test area by a mixing station that injects the required amount of hydrogen into a flowing streaming of air. The hydrogen/air mixture can then be delivered to the point of release within the vehicle by a flexible hose."

*Annex 5, paragraph 3.1.2.2., amend to read:*

- "3.1.2.2. Execution of the test

- (a) Test gas is blown to the hydrogen gas leakage detector;

- (b) Proper function of the warning system is confirmed within 10 seconds when tested with the gas to verify function of the warning;
- (c) The main shut-off valve is confirmed within 10 seconds to be closed when tested with the gas to verify function of the shut-down. For example, the monitoring of the electric power to the shut-off valve or of the sound of the shut-off valve activation may be used to confirm the operation of the main shut-off valve of the hydrogen supply. "

Annex 5, paragraph 3.2.1.3., amend to read:

"3.2.1.3. Prior to the test the vehicle is prepared to simulate remotely controllable hydrogen releases from the hydrogen system. Hydrogen releases may be demonstrated by using external fuel supply without modification of the test vehicle fuel lines. The number, location and flow capacity of the release points downstream of the main hydrogen shut-off valve are defined by the vehicle manufacturer taking worst case leakage scenarios under a single failure condition into account. As a minimum, the total flow of all remotely controlled releases shall be adequate to trigger demonstration of the automatic "warning" and hydrogen shut-off functions. "

Annex 5, paragraph 4.3., amend to read:

"4.3. The measuring section of the measuring device is placed along the centre line of the exhaust gas flow within 100 mm of where the exhaust is released to the atmosphere.

Annex 7, paragraph 1, amend to read:

"1. Modifications to an existing type approval of CHSS may be approved in accordance with the reduced test programme specified in Table 1 below. Deviations to this table may be allowed if equivalent safety can be ensured."

Annex 7, Table 1 and Notes, amend to read:

"Table 1  
Change of Design

Changed Item		Required Tests
Metallic container or liner material		- Initial burst, Initial pressure cycle life - Sequential hydraulic tests - Fire test
Plastic liner material		- Initial pressure cycle life - Sequential hydraulic tests - Sequential pneumatic tests - Fire test
Fiber material <sup>1</sup>		- Initial burst, Initial pressure cycle life - Sequential hydraulic tests - Fire test
Resin material		- Initial burst, Initial pressure cycle life - Sequential hydraulic tests - Fire test
Diameter <sup>2</sup>	≤20%	- Initial burst, Initial pressure cycle life
	>20%	- Initial burst, Initial pressure cycle life - Sequential hydraulic tests - Fire test

Changed Item		Required Tests
Length	≤50%	- Initial burst, Initial pressure cycle life - Fire test <sup>3</sup>
	>50%	- Initial burst, Initial pressure cycle life - Sequential hydraulic tests - Fire test <sup>3</sup>
Coating		- Sequential hydraulic tests - Fire test <sup>4</sup>
Boss <sup>5</sup>	Material, geometry, opening size	- Initial burst, Initial pressure cycle life
	Sealing (liner and/or valve interface)	- Sequential pneumatic tests
Fire protection system		- Fire test
Valve change <sup>6</sup>		- Sequential pneumatic tests - Fire test <sup>7</sup>
Container attachment	Material, geometry	- Sequential hydraulic tests - Fire test <sup>7</sup>

*Notes:*

1. Change of fiber type, e.g., glass to carbon is not applicable. Change of design applies only to changes of materials properties or manufacturer within a fiber type.
2. Only when thickness change is proportional to diameter change.
3. Fire test is not required, provided safety relief devices or device configuration passed the required fire test on a container with equal or greater internal water volume.
4. Fire test required if coating affects fire performance.
5. Tests are not required if the stresses in the neck are equal to the original stresses or reduced by the design change (e.g., reducing the diameter of internal threads, or changing the boss length), the liner to boss interface is not affected, and the original materials are used for boss, liner, and seals.
6. Alternative valve shall be approved in accordance with part II.
7. Fire test not required if TPRD design has not been changed, and the mass of the changed valve is +/- 30 per cent of the original valve.

*Insert new Annex 8, to read:*

## **"Annex 8 – Part 1**

### **Alternative lateral impact test for CHSS mounted at a height of 800 mm or lower**

1. Test conditions  
The CHSS shall be filled with hydrogen or helium to the test pressure agreed between the manufacturer together and the Technical Service. Tests shall be conducted on the CHSS in the position intended for the installation in the vehicle including attachments, brackets and protective structures if applicable. The protective structure shall be defined by the manufacturer. At the manufacturer's discretion and in agreement with the Technical Service the CHSS may be mounted on a complete vehicle or on a representative body unit.
2. Impactor  
The impactor shall comply with the requirements of UN Regulation No. 95, Annex 5.
3. Test procedure  
The speed of the impactor at the moment of impact shall be  $50 \pm 1$  km/h. However, if the test was performed at a higher impact speed and the compressed hydrogen storage system met the requirements, the test shall be considered satisfactory. The impact direction shall be in an angle of  $90^\circ$  to the vehicle longitudinal axis with the barrier centreline aligned with the middle transversal plane of the CHSS in the vehicle longitudinal direction.

## **Annex 8 – Part 2**

### **Alternative lateral impact test for CHSS mounted at a height above 800 mm**

1. Test conditions  
The CHSS shall be filled with hydrogen or helium to the test pressure agreed between the manufacturer together and the Technical Service. Tests shall be conducted on the CHSS in the position intended for the installation in the vehicle including attachments, brackets and protective structures if applicable. The protective structure shall be defined by the manufacturer. At the manufacturer's discretion and in agreement with the Technical Service the CHSS may be mounted on a complete vehicle or on a representative body unit.  
In addition, the vehicle or body unit shall be secured in the manner prescribed for test C in Appendix 1 to annex 3 of UN Regulation No. 29.
2. Impactor  
The impactor shall comply with the requirements of UN Regulation No. 29, Annex 3 Paragraph 5.1 and 5.2.
3. Test procedure  
The impact energy shall equal be to 29,4 kJ. However, if the test was performed at a higher impact energy and the CHSS met the requirements, the test shall be considered satisfactory. The impact direction shall be in an angle of  $90^\circ$  to the vehicle longitudinal with the impactor centred on the intersection line of the

transversal and the longitudinal planes passing through the middle CHSS in each direction."

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